

Kinetics of Cr(III) Adsorption/Desorption at the γ -Al₂O₃/Water Interface by the Pressure-Jump Technique

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Mechanistic information regarding Cr(III) adsorption onto γ -Al₂O₃ was obtained using the triple layer model (TLM) in conjunction with experimental data gathered using the pressure-jump technique. Adsorption data and TLM simulation results suggest the formation of both mono- and bidentate inner-sphere Cr³⁺ or CrOH²⁺ complexes at the surface of γ -Al₂O₃. The mechanism of Cr(III) sorption was interpreted as proton release from surface hydroxyl group(s) followed by the attachment of Cr³⁺ or CrOH²⁺ to form bidentate (SO)₂Cr⁺ and monodentate SOCrOH⁺. The binding constant of Cr³⁺ or CrOH²⁺ with deprotonated reacting site(s) simulated using the TLM and equilibrium sorption data was in excellent agreement with that determined from kinetic results, verifying the proposed reaction mechanisms. © 1994 Academic Press, Inc.

INTRODUCTION

In natural environments, the fate and distribution of metal ions are regulated, in part, via adsorption/desorption and precipitation reactions occurring at the interface between the aqueous solution and minerals such as Fe and/or Al oxides and hydroxides (1, 2). A variety of models has been used to describe the interactions of metal ions and minerals, e.g., the surface complexation model (SCM) by Stumm *et al.* (3) and the triple layer model (TLM) of Leckie and colleagues (4, 5). In general, those models provide a basis for interpreting experimental data; however, the amount of direct evidence available to verify the reaction mechanism is very limited.

Direct information about the surface structure in adsorptive systems can be obtained using the extended X-ray absorption fine structure analysis technique. This technique was employed by Hayes *et al.* (6) to examine selenite and selenate interactions with goethite. Their work provided evidence for the existence of both outer-sphere (selenate) and inner-sphere (selenite) surface complexes, as envisioned in the TLM.

Kinetic methods can be used to obtain information regarding reaction steps and mechanisms. Most traditional batch and flow methods are incapable of providing detailed information regarding processes at the interface, owing to the absence of methods that can detect changes in the system as rapidly as the adsorption reaction proceeds. Relaxation methods, especially the pressure-jump technique, have therefore been applied to study some such systems, e.g., sorption of Pb, Zn, Cu, Co, and Mn ions on aluminum oxide and of anions on goethite (7-11). The kinetic and mechanistic behavior of Cr(III) sorption on aluminum oxides has not yet been extensively investigated.

This study presents the equilibrium and kinetics of Cr(III) sorption onto γ -Al₂O₃. Chromium is commonly used in acid electroplating, tanning, painting, dye and drug manufacturing, and petroleum refining (12). The health and environmental effects of carcinogenic Cr(VI) are well known (13-15). If Fe(II), HSO₃⁻, or another electron donor such as organic matter is present, Cr(VI) can be reduced to Cr(III), which tends to be attenuated in soil by inorganic phases such as phyllosilicates and hydroxides (16, 17).

Cr(III) ions have unusually slow ligand exchange reactions and have a strong tendency to polymerize in solution (18-23). Several investigators have studied the interactions of Cr(III) with Fe/Al oxide surfaces. Leckie *et al.* (23) proposed that CrOH²⁺ sorbs at the water/goethite interface as a monodentate surface complex. Wehrli *et al.* (18) studied the adsorption kinetics of Cr(III) onto aluminum oxide and reported that Cr(III) sorption is a two-step process and that the resulting surface species included bidentate Cr³⁺, monodentate CrOH²⁺, and bidentate CrOH²⁺. Karthein *et al.* (22) used electron spin resonance (ESR) and electron spin-echo spectroscopy (ESEEM) to explore the interactions of Cr(III) complexes (Cr(oxalate)₃³⁺) with hydrous δ -Al₂O₃ and reported the formation of inner-sphere, bidentate adsorption complexes of the forms (SO)₂Cr⁺, (SO)₂Cr(C₂O₄)⁻, and (SO)₂Cr(C₂O₄)₂³⁻.

The results of the present study extend the current knowledge about the complicated adsorption behavior of trivalent Cr(III) onto γ -Al₂O₃. The main objective of this work was

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to explore the interaction of Cr(III) and γ -Al₂O₃ using the pressure-jump technique. Specifically, the overall equilibrium partitioning between Cr(III) and γ -Al₂O₃ is described. The kinetic rate constants and mechanistic information regarding Cr(III) adsorption at the γ -Al₂O₃/water interface were determined using the relaxation method in conjunction with the TLM.

MATERIALS AND METHODS

Materials

All chemicals used in this study were of reagent analytical grade. The stock Cr(III) solution (1×10^{-2} M and pH < 2.9) was prepared by using Cr(NO₃)₃ · 9H₂O and deionized water (Milli-Q). Under these acidic conditions, the formation of Cr(III) polynuclear hydroxo species is not favorable (24). The background electrolyte solutions were adjusted to 0.01, 0.05, and 0.1 M using NaNO₃. The γ -Al₂O₃ obtained from Aerosil Co. (Japan) was first prewashed with 0.1 M NaOH, according to the procedure described by Hohl and Stumm (25). After the prewash, the γ -Al₂O₃ was rinsed with deionized water and dialyzed before use in adsorption experiments.

Experiments

In batch equilibrium experiments, the pH of a suspension containing 3×10^{-3} M total Cr(III) and γ -Al₂O₃ (40 g dm⁻³) was adjusted with concentrated HNO₃ or NaOH to various values in the pH range 3.0–5.0. At each adjusted pH point, a 30-ml suspension was transferred to a polypropylene tube. The pH values of the suspensions were monitored for at least 72 h under an N₂ atmosphere. Once all obvious fluctuation in suspension pH ceased, a further 48-h shaking period under an N₂ atmosphere was performed to ensure that equilibrium was achieved (18). Thereafter, the pH of each suspension was measured, and the solid and liquid were separated by filtration (0.22 μ m, Millipore). The filtrate was acidified for subsequent Cr analysis (atomic absorption, Perkin-Elmer 5000).

For the kinetic experiments, the suspensions prepared in the batch equilibrium experiments were transferred to the sample cell of the pressure-jump apparatus. The temperature was maintained at $25 \pm 0.1^\circ\text{C}$ in both the sample cell and the reference cell (KCl solution). The pressure-jump apparatus was equipped with a conductivity detector and was similar to that used previously by Inoue *et al.* (26). The primary components of the pressure-jump apparatus were the pressure chamber (Photo High Pressure Inc., Japan), Wheatstone bridge circuit (Sea Land Electr. Wave Inc., Japan), and a digital storage oscilloscope (TEK 2224).

In the pressure-jump relaxation experiments, the equilibrium state of the Cr(III)/ γ -Al₂O₃ system was perturbed by raising the system pressure to 100 atm, using a camshaft pressure pump. The high pressure in the autoclave sample

cell was transmitted to the suspension through a plastic membrane located on the cell cap. A piece of brass shimstock was used for pressure control. When the pressure in the autoclave became high enough, the shimstock burst, and the pressure returned to the ambient condition within 100 μ s. At the moment when the shimstock burst, an oscilloscope was triggered to record the changes in system conductivity. The signals recorded by the oscilloscope were digitized and analyzed by a linear regression technique for calculating the reciprocal relaxation time (τ^{-1}). The correlation coefficient (r^2) was required to be greater than 0.92 in order for the computed τ^{-1} to be acceptable.

Model Analysis

A modified TLM was used to simulate the equilibrium distribution of background electrolyte ions and Cr(III) species at the γ -Al₂O₃/water interface. In the modified TLM, metal ions are allowed to form either inner- or outer-sphere surface complexes, and the effect of surface potential upon solution activity is incorporated into the activity coefficient relationship with a single exponential term. The intrinsic reaction constants and other parameters used in the TLM are summarized in Table 1. Part I (Eqs. [1] and [2]) of Table 1 describes protonation of reacting surface sites, and Part II (Eqs. [3] and [4]) describes the formation of complexes between the background electrolyte ions and the surface. Based on previous work by other investigators (18, 22, 23), the interactions of Cr(III) on the surface of γ -Al₂O₃ are assumed to be those shown in Parts III and IV of Table 1. Ion-pair formation at the β -plane (Eqs. [5] and [6]) occurs if Cr³⁺ or a Cr(III) hydrolytic complex reacts with SOH similarly to a background electrolyte. If adsorption of Cr³⁺ or Cr(III) hydrolytic complex is visualized as a chemically specific reaction, the reaction can be expressed as an inner-sphere surface coordination process (Eqs. [7]–[10]). The equilibrium and mass balance equations are solved simultaneously in the TLM. The specific surface area of γ -Al₂O₃ is 100 m²/g, according to the manufacturer. Site density was reported by Peri (27) to be 8 sites/nm². Inner- and outer-plane capacitances were assumed to be 80 and 20 μ F/cm², respectively, as reported by Hayes *et al.* (28). The above parameters were used in the model analysis to determine the best-fit intrinsic constants for the Cr(III)/ γ -Al₂O₃ reaction.

RESULTS AND DISCUSSIONS

Figure 1 shows Cr(III) sorption onto γ -Al₂O₃ as a function of pH under various background electrolyte concentrations (0–0.1 M). Over a range of less than two pH units, sorption of Cr(III) changes from a negligible amount (at pH 3.1) to nearly total removal (at pH 4.8). The effect of background electrolyte concentration on the adsorption of Cr(III) is fairly insignificant. The formation of different inner- and outer-

TABLE 1
TLM Reactions and Equilibrium Expressions for Cr(III) Species

| Reaction (equation) | Intrinsic equilibrium expression/constant |
|---|---|
| (I) Surface protolysis reactions | |
| $\text{SOH}_2^+ = \text{SOH} + \text{H}^+$ | $K_{\text{a1}}^{\text{int}} = \frac{[\text{SOH}][\text{H}^+]}{[\text{SOH}_2^+]} \exp\left(\frac{-\Psi_0 F}{RT}\right) = 10^{-7.2}$ [1] |
| $\text{SOH} = \text{SO}^- + \text{H}^+$ | $K_{\text{a2}}^{\text{int}} = \frac{[\text{SO}^-][\text{H}^+]}{[\text{SOH}]} \exp\left(\frac{-\Psi_0 F}{RT}\right) = 10^{-9.5}$ [2] |
| (II) Electrolyte surface reactions | |
| $\text{SOH} + \text{Na}^+ = \text{SO}^- - \text{Na}^+ + \text{H}^+$ | $K_{\text{Na}^+}^{\text{int}} = \frac{[\text{SO}^- - \text{Na}^+][\text{H}^+]}{[\text{SOH}][\text{Na}^+]} \exp\left[\frac{(\Psi_\beta - \Psi_0)F}{RT}\right] = 10^{-9.1}$ [3] |
| $\text{SOH} + \text{H}^+ + \text{NO}_3^- = \text{SOH}_2^+ - \text{NO}_3^-$ | $K_{\text{NO}_3^-}^{\text{int}} = \frac{[\text{SOH}_2^+ - \text{NO}_3^-]}{[\text{SOH}][\text{H}^+][\text{NO}_3^-]} \exp\left[\frac{(\Psi_0 - \Psi_\beta)F}{RT}\right] = 10^{8.7}$ [4] |
| (III) Outer-sphere surface reactions | |
| $\text{SOH} + \text{Cr}^{3+} = \text{SO}^- - \text{Cr}^{3+} + \text{H}^+$ | $K_{\text{Cr}^{3+}}^{\text{int}} = \frac{[\text{SO}^- - \text{Cr}^{3+}][\text{H}^+]}{[\text{SOH}][\text{Cr}^{3+}]} \exp\left[\frac{(3\Psi_\beta - \Psi_0)F}{RT}\right]$ [5] |
| $\text{SOH} + \text{Cr}^{3+} + \text{H}_2\text{O} = \text{SO}^- - \text{CrOH}^{2+} + 2\text{H}^+$ | $K_{\text{Cr}^{3+}}^{\text{int}} = \frac{[\text{SO}^- - \text{CrOH}^{2+}][\text{H}^+]^2}{[\text{SOH}][\text{Cr}^{3+}]} \exp\left[\frac{(2\Psi_\beta - \Psi_0)F}{RT}\right]$ [6] |
| (IV) Inner-sphere surface reactions | |
| $\text{SOH} + \text{Cr}^{3+} = \text{SOCr}^{2+} + \text{H}^+$ | $K_{\text{Cr}^{3+}}^{\text{int}} = \frac{[\text{SOCr}^{2+}][\text{H}^+]}{[\text{SOH}][\text{Cr}^{3+}]} \exp\left(\frac{2\Psi_0 F}{RT}\right)$ [7] |
| $2\text{SOH} + \text{Cr}^{3+} = (\text{SO})_2\text{Cr}^{2+} + 2\text{H}^+$ | $K_{\text{Cr}^{3+}}^{\text{int}} = \frac{[(\text{SO})_2\text{Cr}^{2+}][\text{H}^+]^2}{[\text{SOH}]^2[\text{Cr}^{3+}]} \exp\left(\frac{\Psi_0 F}{RT}\right)$ [8] |
| $\text{SOH} + \text{Cr}^{3+} + \text{H}_2\text{O} = \text{SOCrOH}^+ + 2\text{H}^+$ | $K_{\text{CrOH}^+}^{\text{int}} = \frac{[\text{SOCrOH}^+][\text{H}^+]^2}{[\text{SOH}][\text{Cr}^{3+}]} \exp\left(\frac{\Psi_0 F}{RT}\right)$ [9] |
| $2\text{SOH} + \text{Cr}^{3+} + \text{H}_2\text{O} = (\text{SO})_2\text{CrOH} + 3\text{H}^+$ | $K_{\text{CrOH}^+}^{\text{int}} = \frac{[(\text{SO})_2\text{CrOH}][\text{H}^+]^3}{[\text{SOH}]^2[\text{Cr}^{3+}]}$ [10] |

sphere complexes of Cr(III) as proposed in Eqs. [5]–[10] was modeled using the Cr(III) adsorption data with no NaNO₃ addition. The formation of ion-pair-like outer-sphere

complexes of SO–Cr²⁺ in Eq. [5] or SO–CrOH⁺ in Eq. [6] was ruled out since the simulation was unable to match the measured pH-adsorption curves (figure not shown).

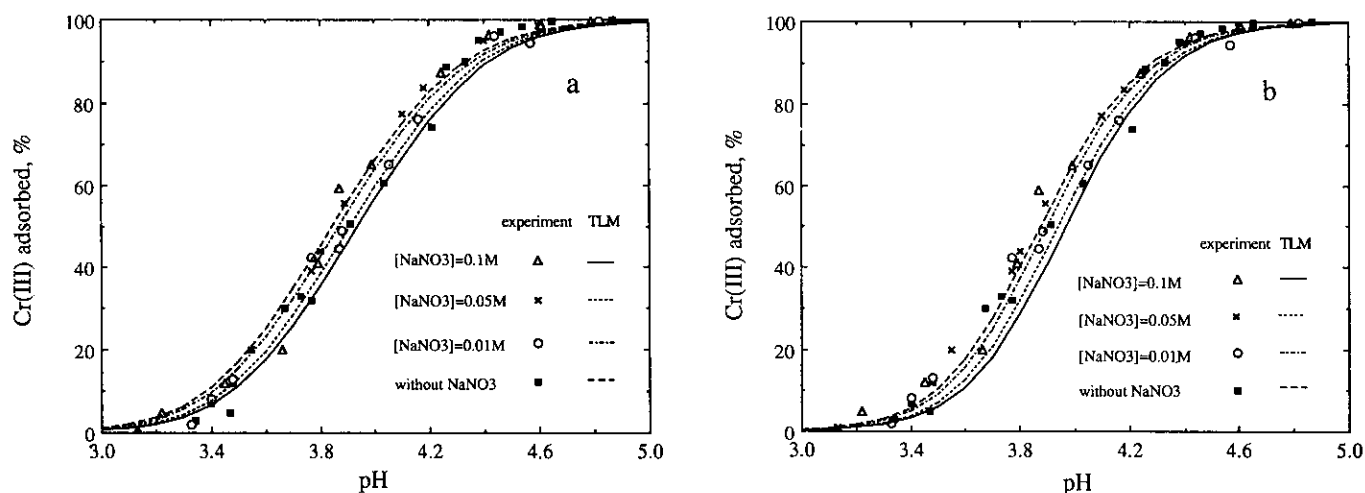


FIG. 1. Adsorption of Cr(III) onto γ -Al₂O₃ as a function of pH under various background NaNO₃ concentrations. Solid and dashed lines denote TLM results. (a) Simulation of monodentate SOCr²⁺ using Eq. [7]. (b) Simulation of bidentate (SO)₂Cr²⁺ using Eq. [8] in Table 1. Symbols denote experimental data.

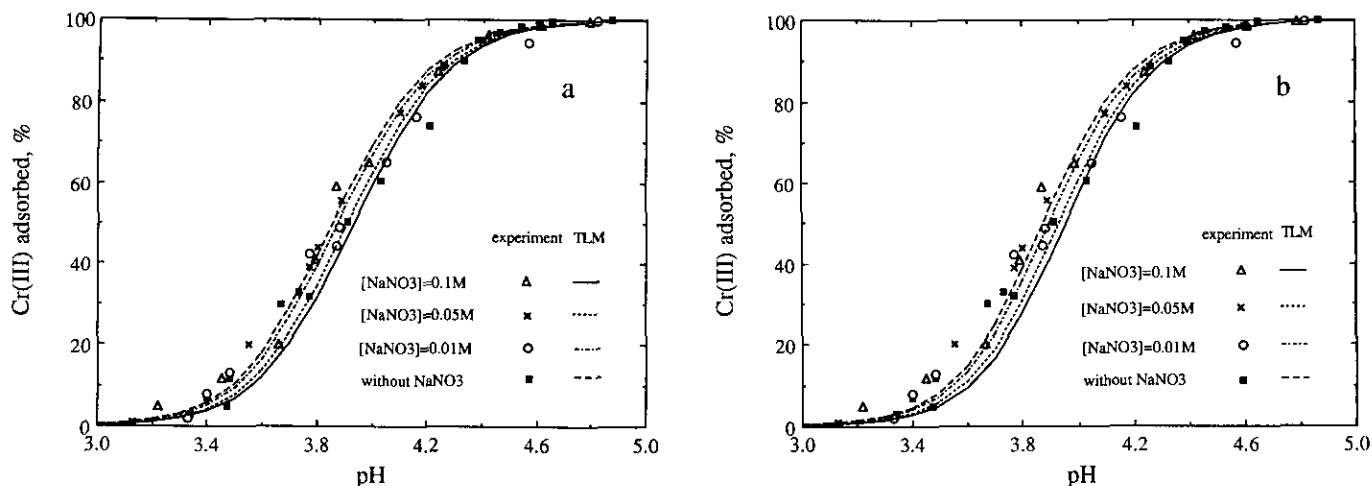


FIG. 2. Adsorption of Cr(III) onto γ - Al_2O_3 as a function of pH under various background NaNO_3 concentrations. Solid and dashed lines denote TLM results. (a) Simulation of monodentate SOCrOH^+ using Eq. [9]. (b) Simulation of bidentate $(\text{SO})_2\text{CrOH}$ using Eq. [10] in Table 1. Symbols denote experimental data.

If it was assumed that the monodentate complex SOCr^{2+} (Eq. [7]) and the bidentate complex $(\text{SO})_2\text{Cr}^+$ (Eq. [8]) formed, the model was able to fit the experimental data quite well (Fig. 1). As the major species in solution over the adsorption pH range are Cr^{3+} and CrOH^{2+} , the formation of monodentate and bidentate Cr(III) hydrolysis species (SOCrOH^+ (Eq. [9]) and $(\text{SO})_2\text{CrOH}$ (Eq. [10])) was also simulated. The model was once again able to fit the experimental data quite well, as shown in Fig. 2.

The negligible effect of background electrolyte concentration on the binding of Cr(III) has been attributed to the formation of inner-sphere surface complexes (5, 29), which is consistent with the simulations shown in Figs. 1 and 2. The formation of all four types of Cr(III) complexes with γ - Al_2O_3 surface was also simulated using the TLM. Figure 3 presents the simulation results, and Table 2 summarizes the respective intrinsic formation constants and the distribution of Cr species at pH 4 and 4.8. The results indicate that bidentate Cr^{3+} and monodentate CrOH^{2+} are the likely dominant species.

Wehrli *et al.* reported that Kurbatov plots indicate that slightly more than two protons are released per Cr(III) adsorbed in the reaction of Cr(III) with aluminum oxide (18). The work of Leckie *et al.* supported the stoichiometric relationship of two protons released with one Cr(III) ion sorbed for CrOH^{2+} adsorption (23). The identity of surface species cannot be proven unequivocally by equilibrium adsorption data and the TLM. However, the stoichiometric relationship and TLM modeling of the Cr(III)/aluminum oxide reaction suggest the formation of bidentate Cr^{3+} or monodentate CrOH^{2+} surface complexes and the presence, at lower concentrations, of monodentate Cr^{3+} and bidentate CrOH^{2+} surface complexes.

Cr(III) aquo ions have a strong tendency to form polynuclear hydroxo species under specific solution conditions

(19–21). Karthein *et al.* employed ESR and ESEEM to study the interaction of Cr(III) complexes with hydrous δ - Al_2O_3 under conditions of total Cr(III) up to $3 \times 10^{-3} \text{ M}$ and pH 4.2 and reported that “chromium complexation at specific surface sites rather than chromium polymer formation takes place” (22). The formation of a bidentate $(\text{SO})_2\text{Cr}(\text{H}_2\text{O})_4$ surface complex was postulated. An X-ray absorption spectroscopic study of the sorption of Cr(III) at the oxide–water interface conducted by Charlet and Manceau (30) showed that small hydroxy polymers might be present at the surface when the Cr(III) surface coverage exceeded about 10% of the active sites. In this work, the Cr(III) sorption density on γ - Al_2O_3 for all the surface species (Eq. [7]–[10]) proposed is calculated to be less than 8% of the total number of reacting sites. Furthermore, the rate of Cr^{3+} dimer and trimer formation is much less than the rate of Cr(III)

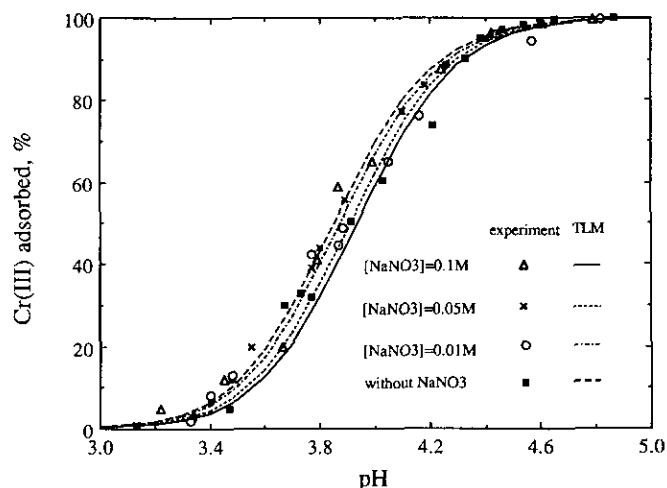


FIG. 3. TLM simulation of mono-/bidentates Cr^{3+} and CrOH^{2+} using Eqs. [7]–[10] in Table 1. Symbols denote experimental data.

TABLE 2
Optimized Intrinsic Formation Constants and Complexed Cr(III) Concentrations from the Simulation of Mono- and Bidentate Formations of Cr³⁺ and CrOH²⁺ Species

| Species | SOCr ²⁺ | (SO) ₂ Cr ⁺ | SOCrOH ⁺ | (SO) ₂ CrOH | Reacted SOH sites/ Total SOH sites ^a |
|----------------------|--------------------------|-----------------------------------|---------------------------|--------------------------|--|
| log K ^{int} | 6.0 | -0.54 | -1.75 | -10.0 | — |
| pH 4 | 2.0 × 10 ⁻⁴ M | 7.0 × 10 ⁻⁴ M | 11.1 × 10 ⁻⁴ M | 0.8 × 10 ⁻⁴ M | 5.4% |
| pH 4.8 | 2.4 × 10 ⁻⁴ M | 10.1 × 10 ⁻⁴ M | 16.1 × 10 ⁻⁴ M | 1.3 × 10 ⁻⁴ M | 7.7% |

^a Total SOH sites: 5.32 × 10⁻² M.

adsorption (22). Therefore, it seems reasonable to discount the formation of Cr(III) polymers on the surface. Based on this assumption, the possible monomeric Cr(III) species sorbed on aluminum oxide were examined by a relaxation method.

A typical relaxation curve is shown in Fig. 4a for the Cr(III)/ γ -Al₂O₃ suspension, using the pressure-jump apparatus with an electrical conductivity detector. The signal recorded in the oscilloscope clearly indicates a decrease in suspension conductivity during the relaxation period. The reciprocal relaxation times (τ^{-1}) can be obtained from the net natural logarithmic plot of the electrical potential versus time, as shown in Fig. 4b. Systems containing Cr(NO₃)₃ only and the supernatant of the suspension of γ -Al₂O₃ were also subjected to the pressure-jump test using the same process. No relaxation was noticed in either of these systems, demonstrating that relaxation can be attributed solely to the

association/dissociation of Cr(III) at the water/ γ -Al₂O₃ interface. The measured reciprocal relaxation times (τ^{-1}) between pH 4 and 4.6 are shown in Fig. 5; τ^{-1} increases with an increase in suspension pH. This trend is consistent with those for other metals (e.g., Pb, Zn, etc.) reported previously (7, 8). The measured τ^{-1} values, suspension pH, ionic strength, activity coefficients, and the percentage of Cr(III) adsorbed, are presented in Table 3.

Proposed reaction pathways in the Cr(III)/ γ -Al₂O₃ system are presented in Table 4. Formation of bidentate Cr³⁺ and monodentate CrOH²⁺ complexes (corresponding to Mechanisms I–IV) were examined. The fast mechanistic pathway proposed by Hachiya *et al.* (8) and Hayes (31) in which the adsorption process is described as an associative mechanism with respect to the exchanged proton is presented as Mechanisms I and II in Table 4. Different possible mechanistic pathways for the adsorption processes were formulated as proton release from surface hydroxyl group(s) followed by attachment of Cr(III) species, as shown in Mechanisms III and IV.

In order to examine the plausibility of the proposed adsorption mechanisms, the corresponding reciprocal relaxation time constants were derived as a function of the reactant

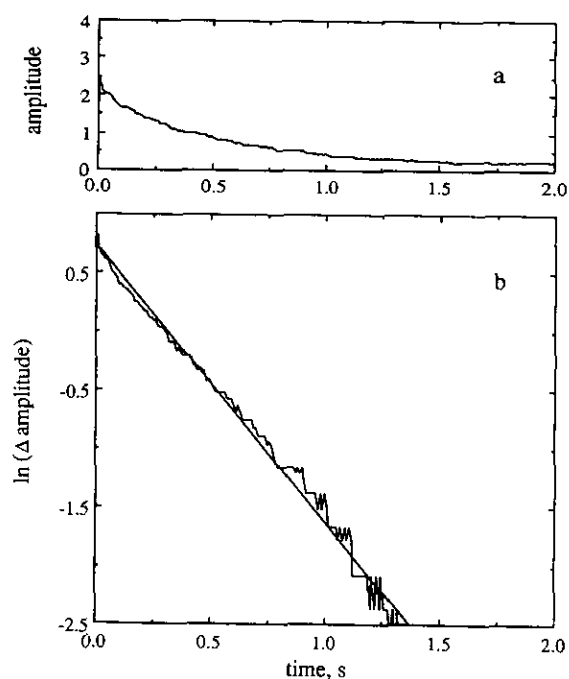


FIG. 4. (a) Typical relaxation curve in Cr(III)/ γ -Al₂O₃ system by the pressure-jump technique at pH 4.32, sweep 0.2 s/div and 25°C. (b) Net natural logarithmic plot of the typical relaxation curve.

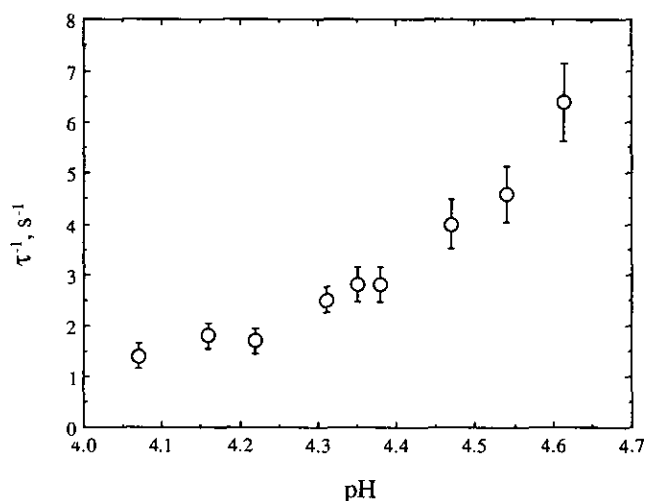


FIG. 5. The pH dependence of reciprocal relaxation time. System contains [γ -Al₂O₃] = 40 g liter⁻¹, [Cr(III)]_T = 3 × 10⁻³ M at 25°C.

TABLE 3
Reciprocal Relaxation Time, Ionic Strength, Ionic Activity, and Chromium (III) Adsorption
as a Function of pH in the Cr(III)/ γ -Al₂O₃ System

| pH | τ^{-1} (s ⁻¹) | I (10 ⁻³ M) | γ (H ⁺) | γ (Cr ³⁺) | γ (CrOH ²⁺) | [Cr(III)] _{ads} (%) |
|------|--------------------------------|--------------------------|----------------------------|------------------------------|--------------------------------|------------------------------|
| 4.07 | 1.4 | 4.28 | 0.938 | 0.588 | 0.774 | 77 |
| 4.16 | 1.8 | 3.43 | 0.943 | 0.592 | 0.792 | 84 |
| 4.22 | 1.7 | 3.01 | 0.946 | 0.608 | 0.802 | 88 |
| 4.31 | 2.5 | 2.59 | 0.949 | 0.627 | 0.813 | 93 |
| 4.35 | 2.8 | 2.49 | 0.950 | 0.633 | 0.816 | 94 |
| 4.38 | 2.8 | 2.41 | 0.951 | 0.636 | 0.818 | 95 |
| 4.47 | 4.0 | 2.28 | 0.952 | 0.644 | 0.822 | 97 |
| 4.54 | 4.6 | 2.22 | 0.952 | 0.647 | 0.824 | 98 |
| 4.62 | 6.4 | 2.20 | 0.953 | 0.648 | 0.824 | 99 |

and product concentrations ($\{M^I\}$, $\{M^{II}\}$, $\{M^{III}\}$, and $\{M^{IV}\}$) for the postulated mechanisms. These constants are also summarized in Table 4. If a plot of τ^{-1} measured from the pressure-jump experiments against the corresponding " $\{M^*\}$ " function calculated from the TLM is linear, the hypothesized mechanism is consistent with the data. The intrinsic reaction rate constant(s) can be determined from the slope or/and intercept of such a plot. Based on such a test, Mechanisms I and II (the Hachiya mechanism) were ruled out, since the corresponding plots were not linear.

Plots of experimentally determined τ^{-1} values versus $\{M^{III}\}$ and $\{M^{IV}\}$ were linear (Figs. 6 and 7), and the slopes and intercepts of the straight lines were used to compute the forward and reverse rate constants of relevant reactions. The intrinsic adsorption equilibrium constants calculated from the kinetic experiments (i.e., the ratio of the forward and reverse reaction rate constants) and the equi-

librium constants simulated from the TLM are listed in Table 5. The equilibrium constants obtained from kinetic experiments (for $(SO)_2Cr^+$, and $SOCrOH^+$ species) are in good agreement with those from equilibrium and the TLM work, indicating that Mechanisms III and IV are reasonable models for the reactions in the Cr(III)/ γ -Al₂O₃ system. The results are consistent with the findings of Karthein *et al.* (22).

Wehrli *et al.* discussed the adsorption kinetics of Cr(III) on δ -Al₂O₃ in batch systems (18). The intrinsic adsorption rate constant of divalent metal ions and their water exchange rates are closely correlated by a linear free-energy relationship (8, 18). Their work suggested that intrinsic adsorption rate constants can be calculated from the water exchange rates of the aquo metal ions. The loss of one water molecule from a metal ion species was believed to be the rate-limiting step for metal sorption. By comparing the water exchange rates of Cr³⁺ and CrOH²⁺ [k_{-w} of CrOH²⁺ is about two orders of magnitude faster (32)] with experimental observations of

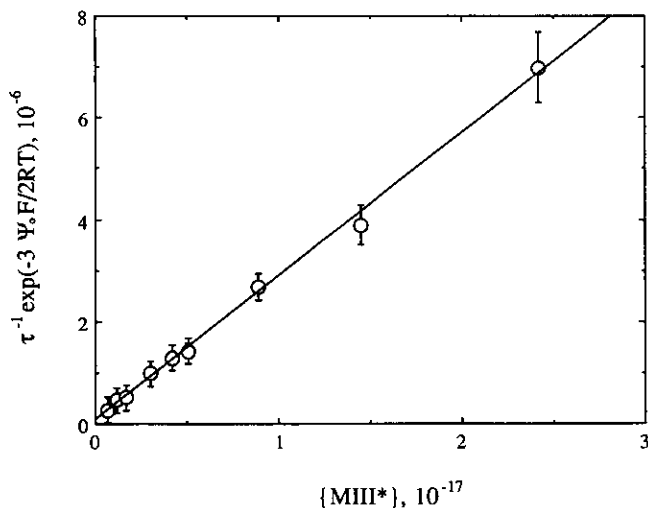


FIG. 6. Plot of $\tau^{-1} \exp(-3\Psi_0 F/2RT)$ vs $\{M^{III}\}$ in Eq. [16]. The concentrations of Cr(III) species were calculated based on the optimized intrinsic formation constants listed in Table 2.

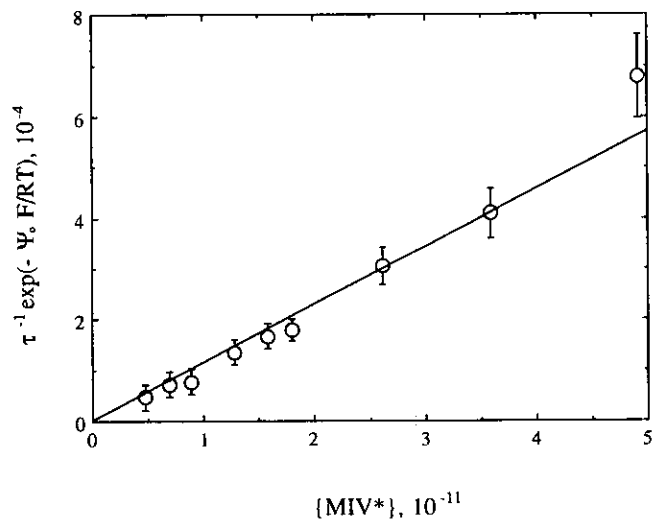


FIG. 7. Plot of $\tau^{-1} \exp(-\Psi_0 F/RT)$ vs $\{M^{IV}\}$ in Eq. [18]. The concentrations of Cr(III) species were calculated based on the optimized intrinsic formation constants listed in Table 2.

TABLE 4
Possible Mechanistic Pathways and the Relationship between Reciprocal Relaxation Times and Concentrations of Cr(III) Species on a γ -Al₂O₃ Surface

| | |
|---|--|
| Mechanism I | |
| (1) Mechanistic pathway | $2\text{SOH} \xrightleftharpoons[k_{-1}]{k_1} 2\text{SOH} \xrightleftharpoons[k_{-2}]{k_2} (\text{SO})_2\text{Cr}^+ \quad [11]$ <div style="display: flex; justify-content: center; gap: 20px; margin-top: -10px;"> <div style="text-align: center;">Cr^{3+}</div> <div style="text-align: center;">Cr^{3+}</div> <div style="text-align: center;">2H^+</div> </div> |
| (2) Relationship between reciprocal relaxation times and species activities | $\tau^{-1} = k_1^{\text{int}} \left\{ \exp\left(\frac{-3\Psi_0 F}{2RT}\right) (\overline{[\text{SOH}]})^2 + \overline{[\text{SOH}]} \overline{[\text{Cr}^{3+}]} \right\} + \frac{1}{K^{\text{int}}} \exp\left(\frac{-\Psi_0 F}{2RT}\right) (\overline{[(\text{SO})_2\text{Cr}^+]}) \overline{[\text{H}^+]} + \overline{[\text{H}^+]}^2 \right\} = k_1^{\text{int}} \{\text{MI}^*\} \quad [12]$ |
| Mechanism II | |
| (1) Mechanistic pathway | $\text{SOH} \xrightleftharpoons[k_{-1}]{k_1} \text{SO} \xrightleftharpoons[k_{-2}]{k_2} \text{SOCrOH}^+ \quad [13]$ <div style="display: flex; justify-content: center; gap: 20px; margin-top: -10px;"> <div style="text-align: center;">CrOH^{2+}</div> <div style="text-align: center;">H^+</div> </div> |
| (2) Relationship between reciprocal relaxation times and species activities | $\tau^{-1} = k_1^{\text{int}} \left\{ \exp\left(\frac{-\Psi_0 F}{RT}\right) (\overline{[\text{SOH}]} + \overline{[\text{CrOH}^{2+}]}) + \frac{1}{K^{\text{int}}} (\overline{[\text{SOCrOH}^+]}) + \overline{[\text{H}^+]} \right\} = k_1^{\text{int}} \{\text{MII}^*\} \quad [14]$ |
| Mechanism III | |
| (1) Mechanistic pathway | $2\text{SOH} \xrightleftharpoons[k_{-1}]{k_1} 2\text{SO}^- \xrightleftharpoons[k_{-2}]{k_2} (\text{SO})_2\text{Cr}^+ \quad [15]$ <div style="display: flex; justify-content: center; gap: 20px; margin-top: -10px;"> <div style="text-align: center;">2H^+</div> <div style="text-align: center;">Cr^{3+}</div> </div> |
| (2) Relationship between reciprocal relaxation times and species activities | $\tau^{-1} \exp\left(\frac{-3\Psi_0 F}{2RT}\right) = k_2^{\text{int}} \left\{ \exp\left(\frac{-3\Psi_0 F}{RT}\right) (\overline{[\text{SO}^-]})^2 + \frac{\overline{[\text{SO}^-]} \overline{[\text{Cr}^{3+}]}}{G} \right\} + k_{-2}^{\text{int}} = k_2^{\text{int}} \{\text{MIII}^*\} + k_{-2}^{\text{int}} \quad [16]$ |
| with | $G \equiv \frac{\overline{[\text{H}^+]}^2 \overline{[\text{SO}^-]}}{(K_{a2}^{\text{int}})^2 \exp(2\Psi_0 F/RT) \overline{[\text{SOH}]} + \overline{[\text{H}^+]} \overline{[\text{SO}^-]}^2} + 1$ |
| Mechanism IV | |
| (1) Mechanistic pathway | $\text{SOH} \xrightleftharpoons[k_{-1}]{k_1} \text{SO}^- \xrightleftharpoons[k_{-2}]{k_2} \text{SOCrOH}^+ \quad [17]$ <div style="display: flex; justify-content: center; gap: 20px; margin-top: -10px;"> <div style="text-align: center;">H^+</div> <div style="text-align: center;">CrOH^{2+}</div> </div> |
| (2) Relationship between reciprocal relaxation times and species concentrations | $\tau^{-1} \exp\left(\frac{-\Psi_0 F}{RT}\right) = k_2^{\text{int}} \left\{ \exp\left(\frac{-2\Psi_0 F}{RT}\right) (\overline{[\text{SO}^-]} + \overline{[\text{CrOH}^{2+}]}) \frac{(K_1^{\text{int}}) \exp(\Psi_0 F/RT) + \overline{[\text{SO}^-]}}{(K_1^{\text{int}}) \exp(\Psi_0 F/RT) + \overline{[\text{H}^+]} \overline{[\text{SO}^-]}} \right\} + k_{-2}^{\text{int}} = k_2^{\text{int}} \{\text{MIV}^*\} + k_{-2}^{\text{int}} \quad [18]$ |

adsorption kinetics, Wehrli *et al.* (18) suggested the formation of CrOH²⁺ complex with the surface of δ -Al₂O₃ (although the formation of bidentate Cr³⁺ is also fairly likely). In this study, the water exchange rates of Cr³⁺ and CrOH²⁺ were used to estimate the intrinsic adsorption rate constants using the linear free-energy relationship of Wehrli *et al.* There

was a significant difference between the calculated rate constants and the rate constant determined by pressure-jump in this work. Similar results were noted in the work of Wehrli *et al.* based on the comparison of the linear free-energy relationship calculated value and their experimental observation. According to Wehrli *et al.*, one explanation for the

TABLE 5
The Intrinsic Rate Constants and Equilibrium Constants
in Mechanism III and IV

| Mechanism | $\log k_2^{\text{int}}$ (L mol ⁻¹ s ⁻¹) | $\log k_2^{\text{int}}$ (s ⁻¹) | $\log K_{2,\text{kinetic}}^{\text{int}}$ (L mol ⁻¹) | $\log K_{2,\text{equili}}^{\text{int}}$ (L mol ⁻¹) |
|-----------|---|---|--|---|
| III | 11.45 ^a | -7.08 | 18.53 ^b | 18.46 ^b |
| IV | 7.06 | -6.20 | 13.26 | 11.85 |

^a Unit: L² mol⁻² s⁻¹.

^b Unit: L² mol⁻².

discrepancy is that the metal center may interact with the surface ligand by coordinating with it before a water molecule is released. In an equivalent solution system, Xu *et al.* have suggested that the complete dissociative loss of an H₂O molecule cannot be the only significant step in the ligand substitution process (32).

SUMMARY

In this work, the pressure-jump technique was used to examine the adsorption kinetics of Cr(III) to γ -Al₂O₃. Although the assumption that (SO)₂Cr⁺ and SOCrOH⁺ form yielded excellent agreement between the thermodynamic and kinetic results, our results still suggest that monodentate Cr³⁺ and bidentate CrOH²⁺ might also be present at the interface. Adsorption of Cr(III) onto γ -Al₂O₃ was unaffected by ionic strength changes. The adsorption of Cr(III) onto γ -Al₂O₃ could be interpreted as a two-step process: proton release from surface hydroxyl group(s) (SOH) followed by attachment of Cr(III) to the deprotonated site(s) of the surface complex. The respective intrinsic forward and reverse reaction rate constants for the bidentate Cr³⁺ and monodentate CrOH²⁺ were determined kinetically.

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