

# Linear network analysis of regenerator in a cyclic-flow system

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A linear dynamics model of Darcy's form for a regenerator is first derived, from which a linear network analysis is employed to study the dynamic response of the regenerator in a cyclic-flow system. It is shown that the dynamic response of the regenerator is determined by the design of the load impedance  $Z_2(s)$ . The amplitude attenuation and phase shift between the mass flow and the pressure wave due to the effects of the regenerator configuration and the load impedance can be clearly seen from the present linear network analysis. It is found that introduction of load impedance will reduce the bandwith of a regenerator and increase the phase lag of the mass flow with respect to the pressure wave.

Keywords: regenerator; linear network model; cyclic-flow system

Nomenclature		$V_{\rm o}$	Volume of reservoir (m <sup>3</sup> )	
		x	Position (m)	
$A_{\mathrm{fr}}$	Flow area in regenerator (m <sup>2</sup> )			
$A_{ m HT}$	Surface area of regenerator (m <sup>2</sup> )	Crask latters		
$C_{\rm v}$	Specific heat of gas at constant volume (J	Greek letters		
	$kg^{-1} K^{-1})$	ρ	Gas density (kg m <sup>-3</sup> )	
$C_{\rm s}$	Specific heat of matrix (J kg <sup>-1</sup> K <sup>-1</sup> )	$ ho_{ m s}$	Matrix density (kg m <sup>-3</sup> )	
	Gas pressure (N m <sup>-2</sup> )	$\mu$	Gas viscosity	
p R	Gas constant $(m^2 K^{-1} s^{-2})$	ν	Kinematic viscosity (m <sup>2</sup> s <sup>-1</sup> )	
	Gas temperature (K)		• • • • • • • • • • • • • • • • • • • •	
$T_{ m f} T_{ m s}$	Matrix temperature (K)			
t	Time (s)	Superscripts		
$V_{ m R}$	Total volume of regenerator (m <sup>3</sup> )	~	Steady state or mean value	
IX.	<b>6</b>	~	Perturbed value	

A regenerator is a cold-storage element in regenerative coolers such as Stirling, pulse-tube and Gifford-McMahon coolers. The transient heat transfer in regenerators has been studied by many researchers<sup>1-5</sup>. Guo<sup>6,7</sup> studied the dynamic response of a regenerator using linear system theory, and a network model and a distributed-parameter model of the regenerator were derived. The studies focused only on the dynamic model of the regenerator. In practice, the regenerator is just one component in a system and the dynamic response of the regenerator should be analysed from the viewpoint of a dynamic system.

Huang and Lu<sup>8</sup> studied the dynamic characteristics of a regenerator connecting an infinite reservoir impedance) and a reciprocating piston at isothermal conditions. Their study was further extended to emulate closely the practical situation in pulse-tube coolers. The dynamic response of a non-isothermal regenerator connecting a load impedance resulting from the flow resistance of a passage and the flow capacitance of a finite reservoir (Figure 1) is studied here using the linear network model.

# Linear perturbation model of regenerator

The regenerator is an energy-storage element made from screen mesh wire or powders. Assuming one-dimensional flow, no axial conduction, an ideal gas, constant properties and an isotropic regenerator, the transient governing equa-

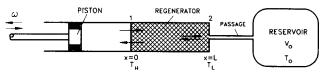


Figure 1 Regenerator system in the present study

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tions can be derived from the conservation of mass, momentum and energy of the gas.

To linearize the governing equations, the inertia terms and the second-order terms in the momentum equations are neglected and a modified frictional coefficient  $\overline{\alpha}$  which varies with the amplitude  $\dot{m}_{\rm max}$  of the oscillating flow, i.e.  $\bar{\alpha}$  $= f(\dot{m}_{\text{max}})$ , is used to account for the pressure loss of the regenerator. The linearly perturbed equations thus can be derived by using the perturbation relations:  $\dot{m}(x,t) = \overline{\dot{m}}(x)$  $+ \dot{m}(x,t); p(x,t) = \overline{p}(x) + \tilde{p}(x,t); T_f(x,t) = \overline{T}_f(x) + \tilde{T}_f(x,t);$  $T_{\rm s}(x,t) = \overline{T}_{\rm s}(x) + \widetilde{T}_{\rm s}(x,t)$ :

Gas continuity equation

$$T_{\text{ave}} \frac{\partial \tilde{p}(x,t)}{\partial t} - p_{\text{ave}} \frac{\partial \tilde{T}_{\text{f}}(x,t)}{\partial t} + \frac{RT_{\text{ave}}^2 \partial \tilde{m}(x,t)}{A_{\text{fr}} \partial x} = 0$$
 (1)

Gas momentum equation

$$L_{\rm F} \frac{\partial \tilde{m}(x,t)}{\partial t} + \frac{\partial \tilde{p}(x,t)}{\partial x} + R_{\rm F} \tilde{m}(x,t) = 0 \tag{2}$$

Gas energy equation

$$\frac{C_{\rm F}}{\gamma} \frac{\partial \tilde{p}(x,t)}{\partial t} + \frac{\partial \tilde{m}(x,t)}{\partial x} + \frac{C_{\rm T}}{\gamma \tau_{\rm g}} \left[ \tilde{T}_{\rm f}(x,t) - \tilde{T}_{\rm s}(x,t) \right] = 0 \tag{3}$$

Regenerator matrix energy equation

$$\tau_{s} \frac{\partial \tilde{T}_{s}(x,t)}{\partial t} + [\tilde{T}_{s}(x,t) - \tilde{T}_{f}(x,t)] = 0 \tag{4}$$

where: the flow capacitance  $C_F = A_{fr}/(RT_{ave})$ ; the thermal capacitance  $C_T = p_{ave} A_{fr} / (RT_{ave}^2)$ ; the flow inductance  $L_F =$  $1/A_{\rm fr}$ ; the flow resistance  $R_{\rm F} = \overline{\alpha} \epsilon \nu / A_{\rm fr}$ ; the gas time constant  $\tau_g = \overline{\rho} \epsilon V_R C_v / (hA_{HT})$ ; the matrix time constant<sup>9</sup>  $\tau_s =$  $\rho_{\rm s}(1-\epsilon)V_{\rm R}C_{\rm s}/(hA_{\rm HT})$ ; and  $\gamma=C_{\rm p}/C_{\rm v}$ .

Solving Equations (1)-(4) by Laplace transform and substituting the following boundary conditions:  $\dot{m}(0,s) =$  $\dot{m}_1(s); \ \dot{m}(L,s) = \dot{m}_2(s); \ \tilde{p}(0,s) = \tilde{p}_1(s); \ \tilde{p}(L,s) = \tilde{p}_2(s), \ \text{we}$ obtain the basic transfer-function model of the regenerator

$$\begin{bmatrix} \tilde{m}_{2}(s) \\ \tilde{p}_{2}(s) \end{bmatrix} = \begin{bmatrix} \cosh[\Gamma_{r}(s)L] & -\frac{1}{Z_{cr}(s)} \sinh[\Gamma_{r}(s)L] \\ -Z_{cr}(s) \sinh[\Gamma_{r}(s)L] & \cosh[\Gamma_{r}(s)L] \end{bmatrix} \times \begin{bmatrix} \tilde{m}_{1}(s) \\ \tilde{p}_{1}(s) \end{bmatrix}$$
(5)

where  $\Gamma_r(s) = \sqrt{sC_{FT}(s)(R_F + sL_F)}$  and  $Z_{cr}(s)$  is the characteristic impedance of the dynamic system defined as  $Z_{cr}(s)$ =  $\Gamma_{\rm r}(s)/[sC_{\rm FT}(s)]$ , where

$$C_{FT}(s) = C_F \frac{1 + \frac{\tau_s}{\tau_g(1 + s\tau_s)}}{\gamma + \frac{\tau_s}{\tau_o(1 + s\tau_s)}}$$
(6)

# Dynamic response of regenerator in a cyclicflow system

The dynamic response of a regenerator as shown in Figure 1 is now considered. The regenerator connects a reciprocating piston at the hot side with a constant temperature  $T_{\rm H}$ and a passage at the cold side with a constant temperature  $T_1$ . The reservoir is at a constant temperature  $T_0$  and has a fixed volume  $V_0$ . This configuration is similar to an orifice pulse-tube cooler, except that the pulse tube and the heat exchangers are not included.

## Load impedance

The passage and the reservoir gives an equivalent circuit as shown in Figure 2. The impedance of the passage includes the resistance  $R_{Ft}(s)$ , inductance  $L_{Ft}(s)$  and capacitance  $C_{\rm Fl}(s)$ . The impedance of the reservoir is dominated by a capacitance  $C_{Fo}(s)$ . An equivalent load impedance  $Z_2(s)$  can be defined at the exit of the regenerator:  $Z_2(s) \equiv$  $\tilde{p}_2(s)/\dot{m}_2(s)$ , as shown in Figure 2.

## Dynamic model of cyclic-flow system

A dynamic model of the regenerator in a cyclic-flow system expressed in Darcy's form is given by

$$G_{m_2\Delta p} = \frac{\tilde{m}_2(s)}{\Delta \tilde{p}(s)}$$

$$= \frac{1}{Z_2(s) \left\{ \cosh[\Gamma_r(s)L] - 1 \right\} + Z_{cr}(s) \sinh[\Gamma_r(s)L]}$$
(7)

where  $\Delta \tilde{p} \equiv \tilde{p}_1 - \tilde{p}_2$ .

#### Effect of load impedance

The dynamic response of the regenerator in a cyclic-flow system is affected by the design of the load impedance  $Z_2(s)$ . For the open end, i.e.  $Z_2(s) = 0$ , the sizes of the passage and the reservoir are infinite. Equation (7) then becomes

$$G_{m_2 \Delta p}(s) = \frac{1}{Z_{cr}(s) \sinh[\Gamma_r(s)L]}$$
 (8)

For the closed end, i.e. the regenerator is blocked and  $Z_2(s)$  $=\infty$ ,  $\dot{m}_2=0$  always.

The design of the passage and the reservoir can be controlled such that  $Z_2(s) = Z_{cr}(s)$ . The transfer function for this load-matching condition then becomes

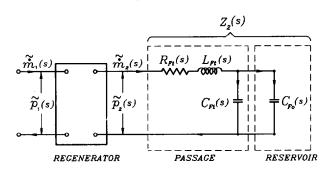


Figure 2 Equivalent circuit of the cyclic-flow system

$$G_{m_2 \Delta p} = \frac{1/Z_{\text{cr}}(s)}{\{\cosh[\Gamma_{\text{r}}(s)L] - 1\} + \sinh[\Gamma_{\text{r}}(s)L]}$$
(9)

#### Dynamic response of regenerator

For illustration, let us assume the following parameters: system mean pressure  $P_{\text{ave}} = 15$  atm (abs);  $T_{\text{H}} = 360$  K;  $T_{\text{L}}$ = 77 K; regenerator average temperature  $T_{\text{ave}}$  = 218.5 K; piston swept volume  $V_P = 6.0 \text{ cm}^3$ ; piston stroke 0.7 cm; piston rod length 2.8 cm; regenerator diameter D = 1.1 cm; and regenerator length L = 5.7 cm. The modified frictional coefficient  $\bar{\alpha}$  is computed using the correlations of Tanaka<sup>10</sup>.  $\overline{\alpha}$  can be presented in terms of the cycle fre-

$$\overline{\alpha} = \frac{175}{2\epsilon d_h^2} + \frac{0.8}{\epsilon d_h \omega} \frac{1.007784 \pi V_p f \rho^*}{A_r \epsilon}$$
 (10)

where:  $\rho^* \equiv \rho(T_{\rm H})/\rho(T_{\rm ave}) = 0.7$  in the present case;  $\epsilon$  is the porosity;  $d_h$  is the hydraulic diameter defined as  $d_h$  =  $\epsilon d_{\rm m}/(1-\epsilon)$ ; and  $d_{\rm m}$  is the wire diameter.

The heat transfer coefficient h inside the regenerator is evaluated by the correlation of Tanaka10

$$h = 0.33 \frac{k_{\rm f}}{d_{\rm h}} \left( \frac{\rho d_{\rm h}}{\mu} \frac{2V_{\rm p} f \rho^*}{A_{\rm r} \epsilon} \right)^{0.67} \tag{11}$$

where:  $A_{\rm HT}/V_{\rm R} = 4(1 - \epsilon)/d_{\rm m}$ ;  $A_{\rm r} = A_{\rm fr}/\epsilon$ ;  $V_{\rm R}$  is the total volume of the regenerator; and  $k_f$  is the thermal conductivity of gas.

Four kinds of stainless screen wire mesh are used: 150, 200, 250 and 400 mesh. The regenerator properties are evaluated using the empirical equations derived by Chang<sup>11</sup>, and are listed in *Table 1*.

The frequency response or Bode plot of  $G_{m_2\Delta p}(s)$  for the open-end configuration  $(Z_2 = 0)$  is presented in Figure 3. The attenuation of  $\dot{m}_2$  as well as the phase shift is larger for the regenerator with a larger mesh number (i.e. denser screen). The bandwidth of  $G_{m_2\Delta p}(j\omega)$  is defined at -3 db gain which specifies the cut-off frequency  $f_{\text{cut}}$ . It is seen from Table 2 that the bandwdith is wider for regenerators with a larger mesh number. However, the phase lags at  $f_{\text{cut}}$ for the four kinds of regenerators are all small and very close, all within 4.2°. This means that a quasi-steady approximation of Darcy's law can hold within the bandwidth, both in terms of gain and phase shift, for the openend configuration  $(Z_2 = 0)$ .

The frequency response or Bode plot of  $G_{m_2\Delta p}(s)$  for the load-matching configuration, i.e.  $Z_2(s) = Z_{cr}(s)$ , is shown in Figure 4. The attenuation of  $\dot{m}_2$  is more rapid for the regenerator with a small mesh number. But the phase lag increases more rapidly with increasing frequency for the

Table 1 Regenerator properties

Mesh	150	200	250	400
d <sub>m</sub> (mm)	0.06604	0.05334	0.04064	0.02540
€	0.732	0.707	0.735	0.686
$d_{\rm b}$ (mm)	0.1803	0.1287	0.1127	0.554
$\alpha$ (mm <sup>-2</sup> )	2691.63	5281.81	6886.6	28 4 17.0
$\beta$ (mm <sup>-1</sup> )	4.437	6.215	7.097	14.417
A <sub>HT</sub> /V <sub>R</sub> (mm <sup>-1</sup> )	16.23	21.97	26.08	52.28

regenerator with large screen wire mesh (i.e. denser screen). It is seen from Table 3 that the bandwidth of  $G_{m_2\Delta p}(j\omega)$  as well as the phase lag increases with increasing mesh number (denser screen). It can be seen from Tables 2 and 3 that the phase lag reaches a minimum value for the open-end configuration and then increases with increasing load impedance  $Z_2(s)$ . This indicates that the flow wave  $\dot{m}_2$  will lag further behind the pressure wave  $\Delta \tilde{p}$  if the load impedance  $Z_2(s)$  increases.

At the load-matching condition, the effect of regenerator impedance vanishes. The pressure as well as the mass flow wave can be propagated directly to the other side of the regenerator without loss. Under this circumstance, the pressure and mass flow wave propagation is determined by the load impedance only. The transport of mass and momentum through the regenerator have the largest efficiency. The load-matching condition is thus the optimum configuration in the cyclic-flow system. The design of the load impedance  $Z_2(s)$  plays an important role in the transport phenomena of waves in the cyclic-flow system of Figure 1.

It can be further shown that for the open-end and loadmatching configurations, the dynamic models in Darcy's form [equations (9)] are reduced to the standard steady state Darcy's equation if the cyclic flow frequency is low. That is

$$\lim_{\omega \to 0} |G_{m_2 \Delta p}(j\omega)| = \frac{A_{\rm fr}}{\overline{\alpha} \epsilon \nu L} = \frac{1}{R_{\rm F} L} = \text{constant}$$
 (12)

This indicates that a quasi-steady approximation of Darcy's law can hold within the bandwidth shown in Tables 2 and 3.

## Realization of load impedance Z<sub>2</sub>(s)

The load impedance  $Z_2(s)$  for the passage and reservoir combination can be realized approximately by the flow resistance  $R_{\rm Ft}$ , the flow capacitance  $C_{\rm Ft}$  and the flow inductance  $L_{Fi}(s)$  of the passage and the flow capacitance  $C_{Fo}(s)$ of the reservoir (see Figure 2). Hence

$$Z_2(s) = R_{Ft} + sL_{Ft} + \frac{1}{s(C_{Ft} + C_{Fo})}$$
 (13)

Here:  $R_{Ft} = f'(L_t/d_t)v/(2A_t)$ ;  $L_{Ft} = L_t/A_t$ ;  $C_{Ft} = A_t L_t/(RT_t)$ ; and  $C_{\text{Fo}} = V_{\text{o}}/(RT_0)$ , where f' is the frictional factor of oscillating pipe flow  $^{12}$ , v is the mean velocity in the passage and A, is the flow area in the passage.

For the load-matching condition  $Z_2(s) = Z_{cr}(s)$ , the dimensions of  $d_t$ ,  $L_t$  and  $V_o$  are evaluated and listed in Table 4. It is seen that for the passage with diameter  $d_1 = 0.5$  mm, the required length  $L_{\rm t}$  varies from 1.22 to 3.65 mm and the reservoir volume V<sub>o</sub> varies from 7.5 to 22.9 cm<sup>3</sup>. The passage in this case looks more like an orifice plate instead of a tube. This situation is quite similar to that of an orifice pulse-tube cooler.

#### Conclusions

A linear dynamic model of Darcy's form for a regenerator is first derived, from which a linear network analysis is employed to study the dynamic response of the regenerator in a cyclic-flow system. It is shown that the dynamic

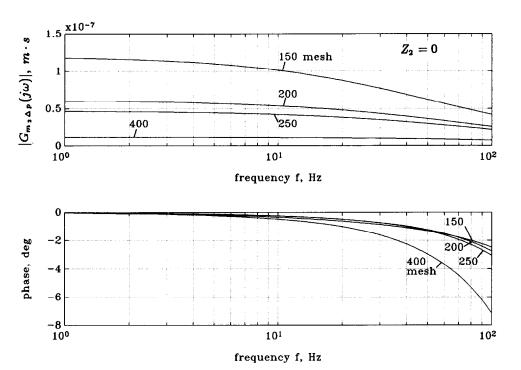


Figure 3 Bode plot of  $G_{m_2\Delta p}(s)$  for open-end configuration ( $Z_2=0$ )

**Table 2** Cut-off frequency of  $G_{m_2\Delta\rho}(j\omega)$  for  $Z_2(s)=0$ 

Mesh	f <sub>cut</sub> (Hz)	φ <sub>cut</sub> (°)	
150	22.0	-0.687	
200	29.7	-0.737	
250	35.2	-0.898	
400	66.6	-4.20	

**Table 3** Cut-off frequency of  $G_{m_2\Delta\rho}(j\omega)$  for  $Z_2(s)=Z_{\rm cr}$  (s)

Mesh	f <sub>cut</sub> (Hz)	$\phi_{ m cut}$ (°)
150	19.1	-2.71
200	23.9	-3.74
250	26.9	-4.48
400	34.4	-9.31

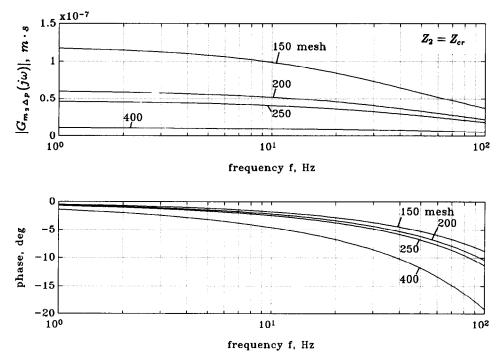


Figure 4 Bode plot of  $G_{m_2\Delta\rho}(s)$  for matched condition  $(Z_2=Z_{cr})$ 

**Table 4** Load configuration for  $Z_2(s) = Z_{cr}(s)$ 

<i>d</i> , (mm)		0.2	0.5	1.0	1.25	2.0
150 mesh	$L_{\rm t}$ (mm) $V_{\rm o}$ (cm <sup>3</sup> )				100.0 20.1	944.0 12.2
200 mesh	$L_{\rm t}$ (mm) $V_{\rm o}$ (cm <sup>3</sup> )				137.0 14.5	1291.0 7.4
250 mesh	$L_{\rm t}$ (mm) $V_{\rm o}$ (cm <sup>3</sup> )					1417.0 5.5
400 mesh	$L_{\rm t}$ (mm) $V_{\rm o}$ (cm <sup>3</sup> )				299.8 6.2	

response of the regenerator is determined by the design of the load impedance  $Z_2(s)$ . The amplitude attenuation and phase shift between the mass flow and the pressure waves due to the effects of regenerator configuration and load impedance can be clearly seen from the present linear network analysis. It is shown that introduction of load impedance will reduce the bandwidth of a regenerator and increase the phase lag of the mass flow with respect to the pressure wave. This could reduce the cooling effect in a cooler, since the phase angle between the mass flow and the pressure (or temperature) waves is not in phase. The amplitude attenuation and the phase shift of the mass flow and the pressure waves due to the effect of the regenerator are clearly shown in the present study. Control of this phenomenon is quite important in the design of regenerative-cycle coolers such as Stirling or pulse-tube coolers.

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#### References

- Rea, S.N. and Smith, J.L., Jr The influence of pressure cycling on thermal regenerators ASME J Eng for Ind (Aug 1967) 563-569
- Quale, E.B. and Smith, J.L., Jr An approximate solution for the thermal performance of a Stirling-engine regenerator ASME J Eng for Power: Ser A (April 1969) No. 2, 109-112
- Modest, M.F. and Tien, C.L. Analysis of real-gas and matrix-conduction effects in cyclic cryogenic regenerators ASME J Heat Transfer (May 1973) 199-205
- Modest, M.F. and Tien, C.L. Thermal analysis of cyclic cryogenic regenerators Int J Heat Mass Transfer (1974) 17 37-49
- Walker, G. and Vasishta, V. Heat transfer and flow friction characteristic of dense-mesh wire-screen Stirling-cycle regenerator Adv Cryog Eng (1970) 16 324-332
- Guo, F.Z. et al. Flow characteristics of a cyclic flow regenerator Cryogenics (1987) 27, 152-155
- Guo, F.Z. Network model of cyclic flow regenerator for Stirling cryocooler Cryogenics (1990) 30 (suppl) 199-205
- Huang, B.J. and Lu, C.W. Dynamic response of regenerator in cyclic flow system Cryogenics (1993) 33 1046-1052
- Wylie, E.B. and Streeter, V.L. Fluid Transients McGraw-Hill Inc., New York, USA (1978)
- Tanaka, M., Yamashita, I. and Chisaka, F. Flow and heat transfer characteristics of Stirling engine regenerator in an oscillating flow JSME Int J: Ser II (1990) 33 283-289
- Chang, W.-S. Porosity and effective thermal conductivity of wire screens ASME J Heat Transfer (1990) 112 5-9
- Roach, P.D. and Bell, K.J. Analysis of pressure drop and heat transfer data from the reversing flow test facility, Argonne National Laboratory Report ANL/MCT-88-2 (May 1989)