

Adsorption Mechanism of Gallium(III) and Indium(III) onto γ -Al₂O₃

CHENG-FANG LIN,^{*1} KUEN-SEN CHANG,[†] CHIA-WEN TSAY,^{*} DAR-YUAN LEE,[‡]
SHANG-LIEN LO,^{*} AND TATSUYA YASUNAGA^{*2}

^{*}Graduate Institute of Environmental Engineering, National Taiwan University, Taipei, Taiwan, 106; [†]Department of Environmental Engineering, National Lien-Ho College of Technology and Commerce, Miao-Li, Taiwan, 360; and [‡]Graduate Institute of Agricultural Chemistry, National Taiwan University, Taipei, Taiwan, 106

Received September 30, 1996; accepted December 12, 1996

The adsorption mechanism of trivalent Ga and In onto γ -Al₂O₃ was investigated using a triple-layer model simulation and pressure-jump technique. Bidentate Ga³⁺ and In³⁺ and monodentate GaOH²⁺/InOH²⁺ are the most likely surface species responsible for Ga(III)/In(III) adsorption. Sorption of Ga(III) and In(III) can be interpreted as an associative process. The adsorption pathway is a two-step mechanism: proton release from surface hydroxyl group(s) followed by coordination of Ga(III)/In(III) species to the deprotonated site(s). Intrinsic adsorption rate constants cannot be estimated with a linear free-energy relationship between the adsorption rate constant and the rate of water exchange, which is developed solely based on the dissociative sorption mechanism of divalent ions. © 1997 Academic Press

Key Words: Ga(III); In(III); γ -Al₂O₃; adsorption; water exchange rate; linear free energy; intrinsic adsorption rate constants.

INTRODUCTION

The transport of heavy metals in the aquatic environment has long been the primary interest of environmental engineers and geochemists. Several studies have reported that the fate and the concentration distribution of metal ions are primarily regulated via adsorption/desorption at the surface of minerals such as Fe and/or Al oxides and hydroxides (1, 2). The surface complexation model by Stumm *et al.* (3) and the triple layer model (TLM) of Leckie and his colleagues (4, 5) have been successfully used to interpret the interactions of metal ions and minerals qualitatively and quantitatively. These two models may address the thermodynamic equilibrium of the interfacial phenomena, but they are not able to reveal the mechanistic pathways of the reactions.

The pressure-jump technique has been used to better understand the kinetic aspect of metal adsorption onto minerals. For example, Hachiya *et al.* (6, 7) employed this approach to investigate the reaction mechanisms of divalent Pb, Zn, Cu, Co, and Mn adsorption at the water/oxide interface, while Hayes and Leckie (5) studied the mechanism of Pb

sorption onto goethite. Zhang and Sparks further (8–10) examined the sorption mechanisms of anions at the water/goethite interface. The results of these works have indicated that inner-sphere surface complexes are formed between the divalent ions and oxide surface hydroxyl sites. The sorption pathways are postulated as a two-step mechanism with a metal ion attached first, followed by the release of a proton from the surface hydroxyl group. Furthermore, the intrinsic adsorption rate constants of divalent metal ions obtained from pressure-jump kinetic experiments are closely related to the water exchange rate of metal ions. Hence, the intrinsic adsorption rate constants can be calculated from the water exchange rate of the aquo metal ions based on the linear free-energy relationship (LFER) of Hachiya (7). Other investigators (11, 12), however, report that the sorption mechanism of Cr(III) exhibits different reaction steps from those postulated by Hachiya and Hayes. The intrinsic adsorption rate constants determined by Wehril *et al.* and Chang *et al.* cannot be predicted by the LFER. Consequently, this study was undertaken to further explore the sorption mechanism(s) of trivalent metal ions and evaluate the plausibility of the LFER on calculating intrinsic adsorption rate constants. Ga(III) and In(III) were used as model ions for kinetic investigation of their adsorption onto γ -Al₂O₃ using the pressure-jump technique.

MATERIALS AND METHODS

Materials

Reagent analytical grade Ga(NO₃)₃ and In(NO₃)₃ · 3H₂O were obtained from Strem Chemicals of USA and Nacalai Tesque of Japan, respectively. The 0.01 M stock solutions of Ga(III) and In(III) were prepared with MilliQ water and the solution was acidified to pH 1.2 to ensure no polymerization. The γ -Al₂O₃ obtained from Aerosil Co. (Japan) was prewashed with 0.1 M NaOH, according to the procedure described by Hohl and Stumm (13). After the prewash, the γ -Al₂O₃ was rinsed with deionized water and dialyzed before use in adsorption experiments.

¹ To whom correspondence should be addressed.

² Visiting scholar.

TABLE 1
TLM Reactions and Equilibrium Expressions for Ga(III)/In(III) Species

Reaction (equation)	Intrinsic equilibrium expression/constant
(I) Surface protolysis reactions	
$\text{SOH}_2^+ = \text{SOH} + \text{H}^+$	$K_{a1}^{\text{int}} = \frac{[\overline{\text{SOH}}][\overline{\text{H}^+}]}{[\overline{\text{SOH}_2^+}]} \exp\left(\frac{-\psi_0 F}{RT}\right) = 10^{-7.2}$ [1]
$\text{SOH} = \text{SO}^- + \text{H}^+$	$K_{a2}^{\text{int}} = \frac{[\overline{\text{SO}^-}][\overline{\text{H}^+}]}{[\overline{\text{SOH}}]} \exp\left(\frac{-\psi_0 F}{RT}\right) = 10^{-9.5}$ [2]
(II) Electrolyte surface reactions	
$\text{SOH} + \text{Na}^+ = \text{SO}^- - \text{Na}^+ + \text{H}^+$	$K_{\text{Na}^+}^{\text{int}} = \frac{[\overline{\text{SO}^- - \text{Na}^+}][\overline{\text{H}^+}]}{[\overline{\text{SOH}}][\overline{\text{Na}^+}]} \exp\left(\frac{(\psi_\beta - \psi_0)F}{RT}\right) = 10^{-9.1}$ [3]
$\text{SOH} + \text{H}^+ + \text{NO}_3^- = \text{SOH}_2^+ - \text{NO}_3^-$	$K_{\text{NO}_3}^{\text{int}} = \frac{[\overline{\text{SOH}_2^+ - \text{NO}_3^-}]}{[\overline{\text{SOH}}][\overline{\text{H}^+}][\overline{\text{NO}_3^-}]} \exp\left[\frac{(\psi_0 - \psi_\beta)F}{RT}\right] = 10^{-8.7}$ [4]
(III) Outer-sphere surface reactions	
$\text{SOH} + \text{Me}^{3+} = \text{SO}^- - \text{Me}^{3+} + \text{H}^+$	$K_{\text{Me}}^{\text{int}} = \frac{[\overline{\text{SO}^- - \text{Me}^{3+}}][\overline{\text{H}^+}]}{[\overline{\text{SOH}}][\overline{\text{Me}^{3+}}]} \exp\left[\frac{3\psi_\beta - \psi_0 F}{RT}\right]$ [5]
$\text{SOH} + \text{Me}^{3+} + \text{H}_2\text{O} = \text{SO}^- - \text{MeOH}^{2+} + 2\text{H}^+$	$K_{\text{Me}}^{\text{int}} = \frac{[\overline{\text{SO}^- - \text{MeOH}^{2+}}][\overline{\text{H}^+}]^2}{[\overline{\text{SOH}}][\overline{\text{Me}^{3+}}]} \exp\left[\frac{(2\psi_\beta - \psi_0)F}{RT}\right]$ [6]
(IV) Inner-sphere surface reactions	
$\text{SOH} + \text{Me}^{3+} = \text{SOMe}^{2+} + \text{H}^+$	$*K_{\text{Me}_1}^{\text{int}} = \frac{[\overline{\text{SOMe}^{2+}}][\overline{\text{H}^+}]}{[\overline{\text{SOH}}][\overline{\text{Me}^{3+}}]} \exp\left(\frac{2\psi_0 F}{RT}\right)$ [7]
$2\text{SOH} + \text{Me}^{3+} = (\text{SO})_2\text{Me}^{2+} + 2\text{H}^+$	$*K_{\text{Me}_2}^{\text{int}} = \frac{[(\overline{\text{SO}})_2\overline{\text{Me}^{2+}}][\overline{\text{H}^+}]^2}{[\overline{\text{SOH}}]^2[\overline{\text{Me}^{3+}}]} \exp\left(\frac{\psi_0 F}{RT}\right)$ [8]
$\text{SOH} + \text{Me}^{3+} + \text{H}_2\text{O} = \text{SOMeOH}^+ + 2\text{H}^+$	$*K_{\text{MeOH}_1}^{\text{int}} = \frac{[\overline{\text{SOMeOH}^+}][\overline{\text{H}^+}]^2}{[\overline{\text{SOH}}][\overline{\text{Me}^{3+}}]} \exp\left(\frac{\psi_0 F}{RT}\right)$ [9]
$2\text{SOH} + \text{Me}^{3+} + \text{H}_2\text{O} = (\text{SO})_2\text{MeOH} + 3\text{H}^+$	$*K_{\text{MeOH}_2}^{\text{int}} = \frac{[(\overline{\text{SO}})_2\overline{\text{MeOH}}][\overline{\text{H}^+}]^3}{[\overline{\text{SOH}}]^2[\overline{\text{Me}^{3+}}]}$ [10]

Note. Me stands for Ga or In.

Sorption Experiments

In batch adsorption experiments, the system contained 3×10^{-3} M total Ga(III) or In(III) and 40 g dm^{-3} of $\gamma\text{-Al}_2\text{O}_3$. The background electrolyte concentrations of the suspensions were adjusted to 0.01, 0.05, and 0.1 M using NaNO_3 . The pH of suspension was adjusted with a small amount of HNO_3 or NaOH to cover the range from pH 1.5 to 3.5 (Ga(III) system) or from pH 2.5 to 4.0 (In(III) system). At each adjusted pH point, a 10 ml aliquot of suspension was transferred to a polypropylene tube under an N_2 atmosphere. Samples were kept at $25 \pm 0.1^\circ\text{C}$ and subjected to shaking for 12 days to ensure that equilibrium was achieved. At the end of the equilibrium period, each suspen-

sion pH was determined and the solid and liquid were separated by filtration ($0.2 \mu\text{m}$, Millipore). Filtrates were acidified for subsequent Ga or In analysis using inductively coupled plasma (Jobin Yvon JY-24).

Kinetic Measurements

The pressure-jump apparatus was used for mechanistic investigation of Ga(III)/ or In(III)/ $\gamma\text{-Al}_2\text{O}_3$ interactions. The samples prepared in batch equilibrium experiments after pH measurement were saved for pressure-jump usages. The temperature of the sample cell and reference cell was maintained at $25 \pm 0.1^\circ\text{C}$. The pressure-jump apparatus equipped with an electrical conductivity detector was similar to that

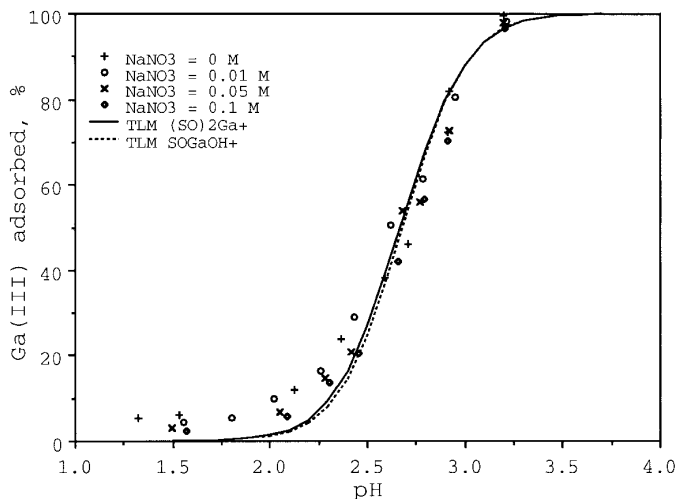


FIG. 1. Adsorption of Ga(III) onto γ -Al₂O₃ as a function of pH under various background NaNO₃ concentrations. Solid line denotes TLM results with no NaNO₃ addition using bidentate (SO)₂Ga⁺ of Eq. [8]. Dotted line represents simulation of monodentate SOGaOH⁺ using Eq. [9]. Symbols denote experimental data.

previously used by Hachiya *et al.* (7). It consisted of a pressure chamber (Photo High Pressure Inc., Japan), a Wheatstone bridge circuit (Sea Land Electr. Wave Inc., Japan), and a digital storage oscilloscope (TEK 2224). During the pressure-jump relaxation measurement, the equilibrium state of the Ga(III)/ or In(III)/ γ -Al₂O₃ system was perturbed by raising the system pressure to approximately 100 atm. The pressure was controlled to return to ambient conditions within 100 μ s. At the moment of pressure change, the oscilloscope was triggered to record the changes in system conductivity. The signals recorded by the oscilloscope were digitized and analyzed by a linear regression technique for calculating the reciprocal relaxation time (τ^{-1}).

Model Analysis

The TLM of Hayes and Leckie (5) was used to simulate the equilibrium distribution of background electrolyte ions and Ga(III) or In(III) species at the γ -Al₂O₃/water interface. The TLM reactions and expression for intrinsic reaction constants are summarized in Table 1. Part I (Eqs. [1] and [2]) of Table 1 describes protonation of reacting surface sites and Part II (Eqs. [3] and [4]) the formation of complexes between the background electrolyte ions and the surface. Based on our recent work (12), the interactions of Ga(III)/In(III) on the surface of γ -Al₂O₃ are assumed to be those shown in Parts III and IV of Table 1. Ion-pair formation at the β -plane (Eqs. [5] and [6]) occurs if Ga³⁺/In³⁺ ion or Ga(III)/In(III) hydrolytic complex reacts with SOH similarly to a background electrolyte. If adsorption of Ga³⁺/In³⁺ or Ga(III)/In(III) complex is visualized as a chemically specific reaction, the reaction can be expressed as an inner-sphere surface coordination process (Eqs. [7]–

[10]). The equilibrium and mass balance equations are solved simultaneously in the TLM. The specific surface area of γ -Al₂O₃ is 100 m²/g, according to the manufacturer. Site density was reported by Peri (14) to be 8 sites/nm². Inner- and outer-plane capacitances were assumed to be 80 and 20 μ F/cm², respectively (15). The above parameters were used in the model analysis to best fit intrinsic constants for the Ga(III)/ or In(III)/ γ -Al₂O₃ reaction.

RESULTS AND DISCUSSION

Equilibrium Adsorption

Adsorption of Ga(III) and In(III) onto γ -Al₂O₃ under various NaNO₃ concentrations are presented in Figs. 1 and 2, respectively. The effect of background electrolyte concentration on the adsorption of Ga(III) and In(III) is insignificant. The pH-adsorption patterns of Ga(III) and In(III) are similar to those of other divalent and trivalent ions. Sorption of Ga(III) changes from a negligible amount at pH 1.5 to nearly total removal at pH 3.0, and the sorption of In(III) covers the range of pH 2.8 to 4.0. Thus, the range of pH-adsorption curves of trivalent metal ions is different from those of divalent metal ions; the trivalent ions are toward the acidic pHs while divalent ions are near the neutral pHs. Specifically, the trend is closely correlated to the first hydrolysis constant (K_1^*) of trivalent ions. The lower the pK_1^* value, the adsorption curve is more toward the acidic pHs. Table 2 lists the pK_1^* values and pH ranges of the adsorption curves of Ga(III), In(III), and Cr(III).

The formation of the outer-sphere complex of Ga(III) or In(III) as proposed in Eqs. [5] and [6] was ruled out as the TLM simulations were unable to match the measured

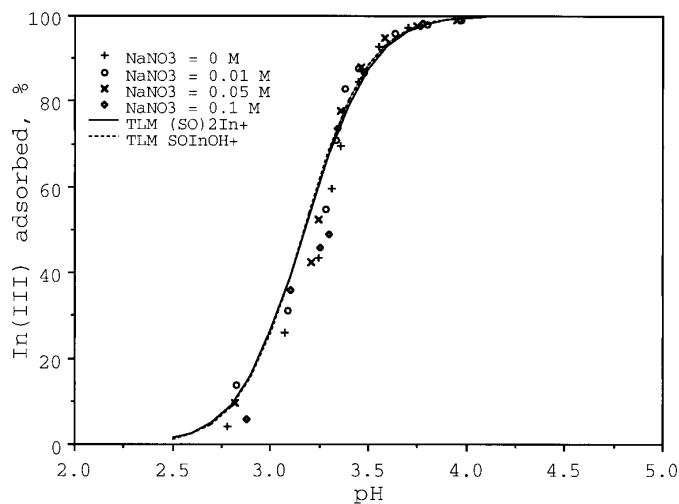


FIG. 2. Adsorption of In(III) onto γ -Al₂O₃ as a function of pH under various background NaNO₃ concentrations. Solid lines denote TLM results with no NaNO₃ addition using bidentate (SO)₂In⁺ of Eq. [8]. Dotted line represents the simulation of monodentate SOInOH⁺ using Eq. [9]. Symbols denote experimental data.

TABLE 2
First Hydrolysis Constant and the pH Adsorption Range of Ga(III), In(III), and Cr(III)

Trivalent metal	pK^*	pH adsorption range
Ga(III)	2.6 ^a	1.5–3.2
In(III)	3.9 ^a	2.8–4.0
Cr(III)	4.1 ^a	3.2–4.5 ^b

^a Baes and Mesmer (18).

^b Chang *et al.* (12).

pH-adsorption curves. Conversely, formation of inner-sphere complexes as proposed in Eqs. [7]–[10] of TLM was able to fit the experimental data with no NaNO₃ addition. Specifically the model was able to fit the data quite well with the formation of the monodentate complex SOGa²⁺ or SOIn²⁺ (figure not shown) and the bidentate complex (SO)₂Ga⁺ [(SO)₂In⁺] as shown in Figs. 1 and 2. As the major Ga(III) and In(III) species over the adsorption pH range are Ga³⁺/In³⁺ and GaOH²⁺/InOH²⁺, the formation of monodentate SOGaOH⁺ [SOInOH⁺] and bidentate (SO)₂GaOH [(SO)₂InOH] was also simulated. The results were also able to fit the experimental data quite well [Fig. 1 (SOGaOH⁺) and Fig. 2 (SOInOH⁺)]. The intrinsic formation constants for the mono- and bidentate Ga(III) and In(III) surface complexes are summarized in Table 3.

The study on Cr(III) adsorption by Chang *et al.* (12) has suggested that the dominant surface species are Cr³⁺ and CrOH²⁺, while Wehril *et al.* (11) report surface CrOH²⁺ species. In the acid/base titration experiments, the calculated number of protons released per Ga(III) or In(III) sorbed is about two (mole basis); for comparison, Wehril *et al.* (11) report slightly more than two protons released per Cr(III) adsorbed onto aluminum oxide. These results may indicate that the formation of monodentate GaOH²⁺/InOH²⁺ and bidentate Ga³⁺/In³⁺ is most likely surface complexes. Indeed, the hypothesis was further verified with the kinetic results using the pressure-jump technique.

TABLE 3
TLM Optimized Intrinsic Formation Constants of Monodentate and Bidentate Ga(III)/In(III) Surface Complexes

Surface complex	Log *K ^{int}
SOGa ²⁺	10.3
(SO) ₂ Ga ⁺	3.15
SOGaOH ⁺	1.73
(SO) ₂ GaOH	-5.21
SOIn ²⁺	8.87
(SO) ₂ In ⁺	1.63
SOInOH ⁺	0.26
(SO) ₂ InOH	-6.67

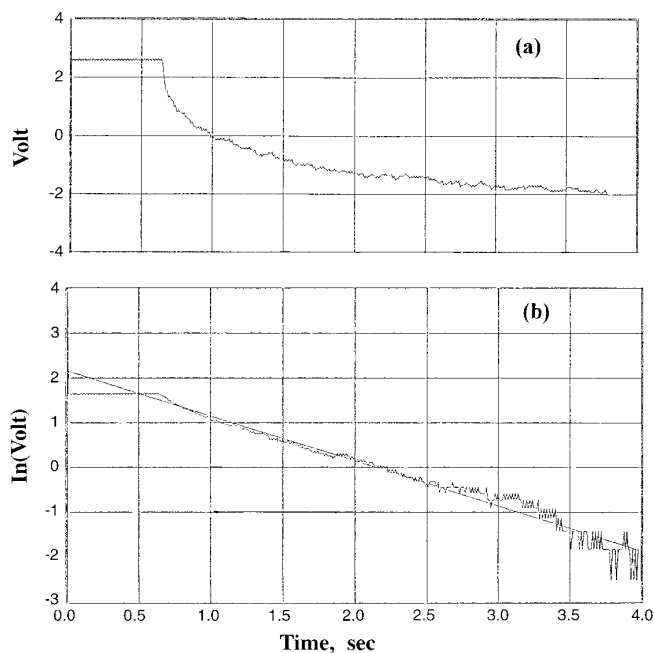


FIG. 3. (a) Typical relaxation curve in Ga(III)/ γ -Al₂O₃ system by pressure-jump technique. (b) Semi-logarithmic plot of typical relaxation curve.

Kinetics

A typical relaxation curve for the Ga(III)/ γ -Al₂O₃ suspension is shown in Fig. 3a. Similar relaxation curves were also observed for the In(III)/ γ -Al₂O₃ suspension. The τ^{-1} was obtained from the natural logarithmic plot of the electrical potential versus time (Fig. 3b). Systems containing Ga(NO₃)₃ or In(NO₃)₃ · 3H₂O only and the supernatant of the suspension of γ -Al₂O₃ were also subjected to the pressure-jump test. No relaxation was noticed in either of these systems, demonstrating that relaxation can be attributed solely to the association/dissociation of Ga(III)/In(III) at the water/ γ -Al₂O₃ interface.

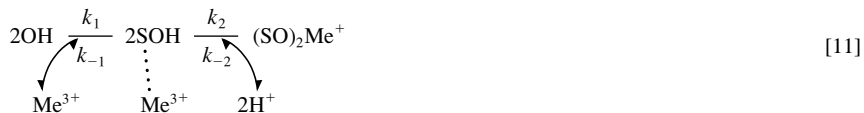
Proposed reaction pathways in the Ga(III) or In(III)/ γ -Al₂O₃ system are presented in Table 4. Mechanisms I and II in Table 4 represent the mechanistic pathway proposed by others (5, 7) in which the sorbed metal ion is associated with surface hydroxyl site(s) followed by the detachment of proton(s). Other possible mechanistic pathways for the adsorption processes were formulated as proton release from surface hydroxyl group(s) followed by attachment of Ga(III)/In(III) species as shown in mechanisms III and IV which are analogous to the S_N1 mechanism (substitution nucleophilic unimolecular) (16).

To examine the plausibility of the proposed adsorption mechanisms, the corresponding reciprocal relaxation time constants were derived as a function of the reactant and product concentrations ($\{MI^*\}$, $\{MII^*\}$, $\{MIII^*\}$, and $\{MIV^*\}$, Table 4) for the postulated mechanisms. If a plot of τ^{-1} measured from the pressure-jump experi-

TABLE 4
Possible Mechanistic Pathways and the Relationship between Reciprocal Relaxation Times and Concentrations of Ga(III)/In(III) Species on a γ -Al₂O₃ Surface

Mechanism I

(1) Mechanistic pathway



(2) Relationship between reciprocal relaxation times and species activities

$$\tau^{-1} = k_1^{\text{int}} \left\{ \exp\left(\frac{-3\psi_0 F}{2RT}\right) (\overline{[\text{SOH}]^2} + \overline{[\text{SOH}]} \overline{\{\text{Me}^{3+}\}}) + \frac{1}{K^{\text{int}}} \exp\left(\frac{-\psi_0 F}{2RT}\right) (\overline{[(\text{SO})_2\text{Me}^+]} \overline{\{\text{H}^+\}} + \overline{\{\text{H}^+\}^2}) \right\} = k_1^{\text{int}} \{\text{MI}^*\} \quad [12]$$

Mechanism II

(1) Mechanistic pathway



(2) Relationship between reciprocal relaxation times and species activities

$$\tau^{-1} = k_1^{\text{int}} \left\{ \exp\left(\frac{-\psi_0 F}{RT}\right) (\overline{[\text{SOH}]} + \overline{\{\text{MeOH}^{2+}\}}) + \frac{1}{K^{\text{int}}} (\overline{[\text{SOMeOH}^+]} + \overline{\{\text{H}^+\}^2}) \right\} = k_1^{\text{int}} \{\text{MII}^*\} \quad [14]$$

Mechanism III

(1) Mechanistic pathway



(2) Relationship between reciprocal relaxation times and species activities

$$\tau^{-1} \exp\left(\frac{-3\psi_0 F}{2RT}\right) = k_2^{\text{int}} \left\{ \exp\left(\frac{-3\psi_0 F}{RT}\right) (\overline{[\text{SO}^-]^2} + \frac{\overline{[\text{SO}^-]} \overline{\{\text{Me}^{3+}\}}}{G}) \right\} + k_{-2}^{\text{int}} = k_2^{\text{int}} \{\text{MIII}^*\} + k_{-2}^{\text{int}} \quad [16]$$

with

$$G = \frac{\overline{\{\text{H}^+\}^2} \overline{[\text{SO}^-]}}{(K_{a2}^{\text{int}})^2 \exp(2\psi_0 F/RT) \overline{[\text{SOH}]} + \overline{\{\text{H}^+\}} \overline{[\text{SO}^-]^2}} + 1$$

Mechanism IV

(1) Mechanistic pathway



(2) Relationship between reciprocal relaxation times and species activities

$$\tau^{-1} \exp\left(\frac{-\psi_0 F}{RT}\right) = k_2^{\text{int}} \left\{ \exp\left(\frac{-2\psi_0 F}{RT}\right) (\overline{[\text{SO}^-]} + \overline{\{\text{MeOH}^{2+}\}}) \frac{(K_{a2}^{\text{int}} \exp(\psi_0 F/RT) + \overline{[\text{SO}^-]})}{(K_{a2}^{\text{int}} \exp(\psi_0 F/RT) + \overline{\{\text{H}^+\}} \overline{[\text{SO}^-]})} \right\} + k_{-2}^{\text{int}} = k_2^{\text{int}} \{\text{MIV}^*\} + k_{-2}^{\text{int}} \quad [18]$$

Note. Me denotes Ga or In.

TABLE 5
The Intrinsic Rate Constants and Equilibrium Constants
in Mechanism III and IV

Mechanism	Log $*k_2^{\text{int}}$ (L mol ⁻¹ s ⁻¹)	Log $*k_{-2}^{\text{int}}$ (s ⁻¹)	Log $*K_{2,\text{kinetic}}^{\text{int}}$ (L mol ⁻¹)	Log $*K_{2,\text{equilibrium}}^{\text{int}}$ (L mol ⁻¹)	
Ga	III	13.22	-8.92	22.13	22.15
	IV	8.04	-6.39	14.43	13.83
In	III	12.83	-8.96	21.34	20.63
	IV	7.44	-8.06	15.49	13.76

ments against the corresponding “{M*}” function calculated from the TLM is linear, the hypothesized mechanism is consistent with the data. The intrinsic reaction rate constants are then determined from the slope and/or intercept of such a plot. As a result, mechanisms I and II (the Hachiya mechanism) were ruled out, since the corresponding plots were not linear.

Plots of experimentally determined τ^{-1} values versus {MIII*} and {MIV*} were linear (Figs. 4 and 5 for Ga(III)/ γ -Al₂O₃; Figs. 6 and 7 for In(III)/ γ -Al₂O₃), and the slopes and intercepts of the straight lines were used to compute the forward and reverse rate constants of relevant reactions. The intrinsic adsorption equilibrium constants calculated from the kinetic experiments (i.e., the ratio of the forward and reverse reaction rate constants) and the equilibrium constants simulated from the TLM are listed in Table 5 for comparison. These constant values obtained from kinetic experiments (for (SO)₂Ga⁺ [(SO)₂In⁺], and SOGaOH⁺ [SOInOH⁺] species) are in good agreement with those from equilibrium and the TLM work, indicating that mechanisms III and IV are

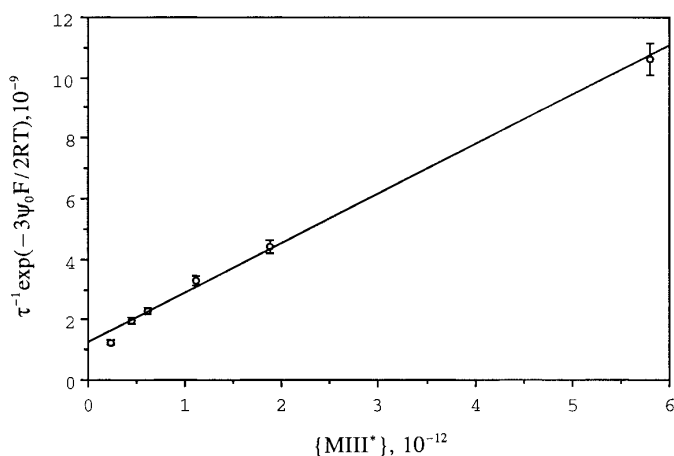


FIG. 4. Plot of $\tau^{-1}\exp(-3\psi_0F/2RT)$ vs {MIII*} in Eq. [16]. The concentrations of Ga(III) species were calculated based on the optimized intrinsic formation constants.

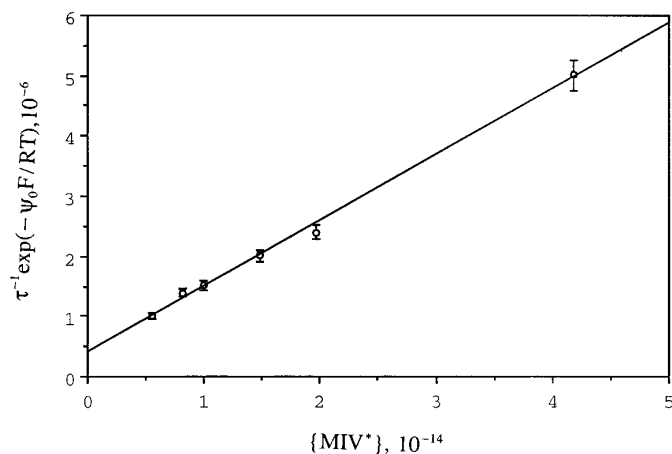


FIG. 5. Plot of $\tau^{-1}\exp(-\psi_0F/RT)$ vs {MIV*} in Eq. [18]. The concentrations of Ga(III) species were calculated based on the optimized intrinsic formation constants.

reasonable models for the reactions in the Ga(III)/ or In(III)/ γ -Al₂O₃ system.

Hachiya *et al.* (7) applied the pressure-jump technique to study the adsorption mechanism of Pb²⁺, Cu²⁺, Zn²⁺, Co²⁺, and Mn²⁺ and reported that the adsorption of divalent metal ions exhibited the dissociative mechanism. The sorption process is stated as a two-step ligand exchange reaction in which the hydrated metal ion exchanges with the proton on oxide surface. In the first step, the hydrated metal ion loses one water molecular before it can attach to the surface hydroxyl reacting site. Thereafter, a proton is released to be substituted by the hydrated metal (Fig. 8a). As the surface reacting group does not affect the exchange rate, the reaction rate-limiting step might be closely correlated to the dissociation of hydrated water, i.e., the water exchange rate ($k_{\text{H}_2\text{O}}$). The LFER between the intrinsic adsorption rate constant, $k_{\text{ads(int)}}$,

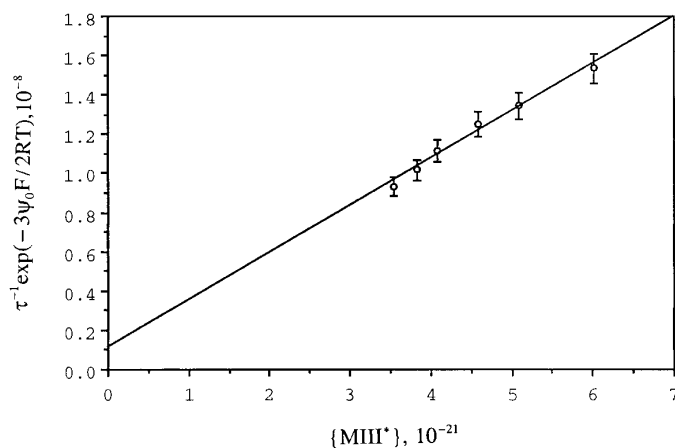


FIG. 6. Plot of $\tau^{-1}\exp(-3\psi_0F/2RT)$ vs {MIII*} in Eq. [16]. The concentrations of In(III) species were calculated based on the optimized intrinsic formation constants.

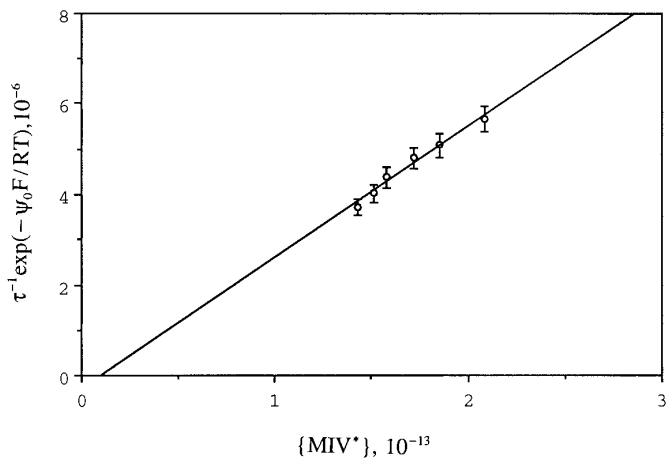


FIG. 7. Plot of $\tau^{-1}\exp(-\psi_0 F/RT)$ vs $\{MIV^*\}$ in Eq. [18]. The concentrations of In(III) species were calculated based on the optimized intrinsic formation constants.

and k_{H_2O} is $\log k_{ads(int)} = -4.16 + 0.92 \log k_{H_2O}$. Stumm (17) also notes that trivalent ions of Fe^{3+} and Al^{3+} follow this relationship. By substituting the water exchange rates of Ga^{3+} and In^{3+} (7.6×10^2 and 4.0×10^4 (18)) into the above equation, it is found that there exists a discrepancy between the estimated $k_{ads(int)}$ and the pressure-jump determined values.

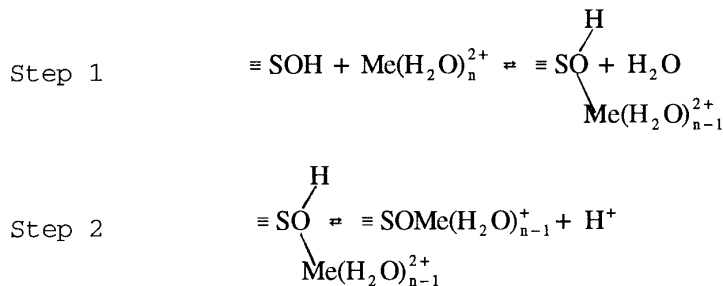
Wehril *et al.* (11) proposed that Cr^{3+} sorption was an associative mechanism and also noted that the adsorption rate constant was not comparable to that estimated by

LFER. In our recent work (12), the adsorption pathway of $Cr(III)/\gamma-Al_2O_3$ was different from that proposed by Hachiya *et al.* (7) and Wehril *et al.* (11). Although $Cr(III)$ sorption is an associative process, Chang *et al.* (12) interpreted that a proton is released from surface hydroxyl group(s) followed by the attachment of $Cr(III)$ species. The results of the present study essentially present the similar adsorption mechanisms of trivalent Ga and In ions onto $\gamma-Al_2O_3$ (Fig. 8b). Thus, the hydrated water interactions with the cation and surface sites are more rapid than those of the adsorption reaction and, as a result, hydration rate evaluation is not possible.

CONCLUSIONS

Kinetic investigation of Ga(III) and In(III) sorption on $\gamma-Al_2O_3$ indicates that the adsorption pathway of trivalent ions is a two-step mechanism: proton release from surface hydroxyl group(s) followed by coordination of Ga(III)/In(III) species to the deprotonated site(s). Formation of monodentate $SOGaOH^+/SOInOH^+$ and bidentate $(SO)_2Ga^+/(SO)_2In^+$ are the likely surface complexes which were verified by the pressure-jump results. The intrinsic adsorption rate constants for the Ga(III) and In(III) species were determined kinetically. The sorption of trivalent metal ions is an associative processes; therefore it is not possible to estimate the sorption rate constant with the LFER which is appropriate only for divalent metal ions.

(a) Divalent metal ion



(b) Trivalent metal ion

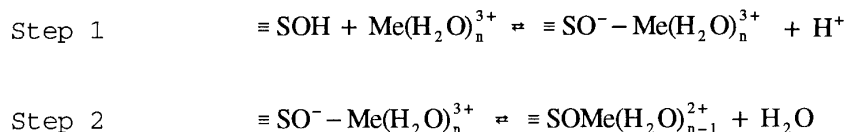


FIG. 8. Sorption mechanism of (a) divalent and (b) trivalent metal ions.

ACKNOWLEDGMENT

Funding for this research was provided by the National Science Council of the Republic of China under Grant NSC 83-0410-E-002-082.

REFERENCES

1. Huang, C. P., and Stumm, W., *J. Colloid Interface Sci.* **34**, 409 (1973).
2. Benjamin, M. M., *Environ. Sci. Technol.* **17**, 686 (1983).
3. Stumm, W., Huang, C. P., and Jenkins, S. R., *Croat. Chem. Acta* **42**, 223 (1970).
4. Davis, J. A., and Leckie, J. O., *J. Colloid Interface Sci.* **67**, 90 (1978).
5. Hayes, K. F., and Leckie, J. O., *J. Colloid Interface Sci.* **115**, 564 (1987).
6. Hachiya, K., Ashida, M., Sasaki, M., Kan, H., Inoue, T., and Yasunaga, T., *J. Phys. Chem.* **83**, 1866 (1979).
7. Hachiya, K., Sasaki, M., Saruta, Y., Mikami, N., and Yasunaga, T., *J. Phys. Chem.* **88**, 23 (1984).
8. Zhang, P. C., and Sparks, D. L., *Soil Sci. Am. J.* **53**, 1028 (1989).
9. Zhang, P. C., and Sparks, D. L., *Environ. Sci. Technol.* **24**, 1848 (1990).
10. Zhang, P. C., and Sparks, D. L., *Soil Sci. Am. J.* **54**, 1266 (1990).
11. Wehrli, B., Ibric, S., and Stumm, W., *Colloids Surf.* **51**, 77 (1990).
12. Chang, K-S., Lin, C-F., Lee, D-Y., Lo, S-L., and Yasunaga, T., *J. Colloid Interface Sci.* **165**, 169 (1994).
13. Hohl, H., and Stumm, W., *J. Colloid Interface Sci.* **55**, 281 (1976).
14. Peri, J. B., *J. Phys. Chem.* **69**, 211 (1965).
15. Hayes, K. F., Redden, G., Ela, W., and Leckie, J. O., *J. Colloid Interface Sci.* **142**, 448 (1991).
16. March, J., "Advanced Organic Chemistry: Reactions, Mechanism, and Structure." McGraw-Hill, New York, 1968.
17. Stumm, W., "Chemistry of the Solid-Water Interface." Wiley, New York, 1992.
18. Martell, A. E., "Coordination Chemistry." American Chemical Society Monograph, Am. Chem. Soc., Washington, D.C., 1978; Baes, C. F., and Mesmer, J. R. E., "The Hydrolysis of Cations." Wiley, New York, 1976.