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控制系統之性能評估與線上監控(2/3)

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控制系統之性能評估與線上監控 (2/3)

Performance Assessment and On-line Monitoring of Control Systems (2/3)

摘要

在本計畫之上一期研究中，針對不同之控制目標，探討了單環路控制系統之性能評估方式。而性能評估必須以程序之低階模式為基礎，因此本期計畫之重點在於程序模式之識別，尤其是程序之等效時延部分。此識別方法利用繼電器回饋測試得到的資料，並配合上類神經網路，可以準確的估計出程序二階模式之等效時延，進而判別此程序應該用 FOPDT 或 SOPDT 模式來表示，然後計算出對應模式之參數。此模式可以用於系統之性能評估與線上監控，此外，更可應用於控制器之調諧，成為一個自動調諧系統並且有效地改善控制系統之性能。

關鍵詞： 控制性能評估、繼電器回饋測試、等效時延、人工類神經網路、自動調諧

Abstract

The previous project has investigated the performance assessment of single-loop control systems. Such assessment is based on the low-order models of the processes. Therefore, this project mainly deals with the identification of the process, especially for the apparent deadtime. The identification method uses the relay feedback test and artificial neural network (ANN) to estimate the apparent deadtime first. Then, the processes are classified to be represented as FOPDT or SOPDT models, and the model parameters are estimated accordingly. The identified models can be used not only for performance assessment but also for controller tuning. It becomes an auto-tuning system and can improve control performance effectively.

Keywords: control performance assessment, relay feedback test, apparent deadtime, artificial neural network, auto-tuning

Introduction

The control performance which a PI/PID control system can achieve depends on the dynamics of the process being controlled (Huang and Jeng, 2002). Thus, a reliable process model is essential to the success of control performance assessment. This project focuses on the identification of such low-order models (FOPDT and SOPDT) for performance assessment.

In 1984, Astrom and Hagglund (1984) presented a relay feedback system to generate sustained oscillation for controller tuning. As shown in Fig. 1(a) is the block diagram of the relay feedback loop. Fig. 1(b) illustrates the typical response curves from the relay feedback system. Because this test is operated under closed-loop and no *a priori* knowledge of the system is need, it has been often adopted for the identification of low-order model of process in the literature. Nevertheless, according to those reports in the literature, the apparent deadtime is usually read from the initial output response or computed using the ultimate information (e.g. Li *et al.*, 1991). The results thus obtained are very rough, and estimation errors may be very large for high-order processes. In addition, due to only frequency-domain information being extracted from the test, more than one relay feedback test is usually required to provide sufficient information for

identification (e.g. Scali *et al.*, 1999).

In this project, a new identification method for performance assessment using the relay feedback test is proposed. The steady-state gain and ultimate controller gain are estimated along with the experiment until constant cycling occurs. The constant cycles at the output and a prepared neural network are then used to estimate the apparent deadtime. Once the apparent is obtained, the process is classified to be represented as FOPDT or SOPDT model using the normalized amplitude and period of constant output cycles. After classifying, the model parameters are estimated accordingly. With the identified model, the performance assessment and controller tuning can proceed.

Process Identification using Relay Feedback Test

The models considered for performance assessment are FOPDT and SOPDT of the following:

- FOPDT
$$G_p(s) = \frac{k_p e^{-\theta s}}{\tau s + 1} \quad (1)$$

- SOPDT
$$G_p(s) = \frac{k_p e^{-\theta s}}{\tau^2 s^2 + 2\tau\zeta s + 1} \quad (2)$$

These two models can be used to represent most open-loop stable processes. In general, overdamped or slightly underdamped processes can be modeled as FOPDT, whereas significantly underdamped processes have to be modeled as SOPDT.

A relay feedback response is used to develop such parametric models. As shown in Fig. 1(a) is a relay feedback system which consists of process, G_p , and a relay controller. The relay controller provides output at $+h$ or $-h$ only as on-off control. The controlled process output consists of transient oscillations after a pure deadtime, θ^o , and develops constant cycling with magnitude, A , and period, P_u . Notice that A and P_u are used in the auto-tuning system of Astrom and Hagglund (1984) to apply Z-N method to compute the PI/PID controller parameters. In the meantime, T_p , θ and an associated height, A_θ , within one of the constant cycles are also indicated in Fig. 1(b). Here, θ is used to designate an apparent deadtime in the FOPDT or SOPDT model, which is used to represent the dynamics of higher order processes. All these quantities measured from a relay feedback response are governed by the dynamic model and the relay. In other words, they can be expressed as:

$$\frac{A}{k_p h} = f_1(\bar{\tau}) \quad \text{or} \quad f_1(\bar{\tau}, \zeta) \quad (3)$$

$$\frac{P_u}{\theta} = f_2(\bar{\tau}) \quad \text{or} \quad f_2(\bar{\tau}, \zeta) \quad (4)$$

$$\frac{A_\theta}{A} = f_3(\bar{\tau}) \quad \text{or} \quad f_3(\bar{\tau}, \zeta) \quad (5)$$

$$\frac{\theta}{T_p} = f_4(\bar{\tau}) \quad \text{or} \quad f_4(\bar{\tau}, \zeta) \quad (6)$$

where $\bar{\tau}$ represents $\bar{\tau} / \theta$. The equations given above describe the dynamic features of the relay

feedback response in time domain. Two equations which correspond to Eqs.(3) and (4) derived from frequency domain are:

$$\omega_u \theta + \tan^{-1} \left(\frac{2\omega_u \tau \zeta}{1 - \omega_u^2 \tau^2} \right) = \pi \quad (7)$$

$$\frac{k_p}{\sqrt{(1 - \omega_u^2 \tau^2)^2 + 4\omega_u^2 \tau^2 \zeta^2}} = \frac{1}{k_{cu}} \quad (8)$$

where ω_u is taken as $2\pi/P_u$. Theoretically, provided that k_p and k_{cu} are given, the identification problem to find an reduced order SOPDT model can be solved by finding τ , ζ , and θ that fit Eqs.(3)-(6) or Eqs.(5)-(8) in the sense of least-squares. The explicit functional forms for Eqs.(3)-(6) are not available, and numerical method to solve the above equations will not be convenient. In the following, a simplified algorithm will be presented to estimate these required data from relay feedback test.

- *Estimation of k_p and k_{cu}*

To estimate k_p , the experimental relay feedback test is started with a temporal disturbance to either the set-point or the process input (i.e. u) for a short period of time and restored back to its origin. The disturbance introduced has two main purposes. One is to initialize the relay feedback control, and the other one is to generate data for computing the steady-state process gain. The estimation is made along the relay feedback test in one run as the following. Let y^I and u^I designate the integrations of y and u from the very beginning of the experiment in one run. That is:

$$y^I(t) = \int_0^t y(\tau) d\tau; \quad u^I(t) = \int_0^t u(\tau) d\tau \quad (9)$$

For some $t > T$ when y in relay feedback test starts to oscillate with constant period and amplitude, y^I and u^I will have similar cycling responses. Typical curves of y^I and u^I are shown in Fig. 2. Let y_{av}^I and u_{av}^I designate the average heights of constant cycles of y^I and u^I , respectively. The value of k_p can be estimated as:

$$k_p = \frac{y_{av}^I}{u_{av}^I} \quad (10)$$

On the other hand, due to the use of describing function for estimation, the ultimate gain computed from $k_{cu} = 4h/\pi A$ is subjected to error, which may, sometimes, be as high as 20%. In order to give more accurate k_{cu} , the following estimation step is considered. Since $u(t)$ and $y(t)$ are periodic with period P_u , they can be expanded into Fourier series. If the first harmonics are extracted, their coefficients give one point of process frequency response at ultimate frequency ω_u via the following equation:

$$G_p(j\omega_u) = \frac{\int_{t_0}^{t_0+P_u} y(t) e^{-j\omega_u t} dt}{\int_{t_0}^{t_0+P_u} u(t) e^{-j\omega_u t} dt} \quad (11)$$

where t_0 is taken as any time instant in a constant cycle. Then, the ultimate gain can be computed exactly as:

$$k_{cu} = \frac{1}{|G_p(j\omega_u)|} \quad (12)$$

- *Estimation of apparent deadtime θ*

The apparent deadtime is the deadtime appearing in an FOPDT or SOPDT model that approximates best the higher order process. As a result, this apparent deadtime differs, in general, from its true deadtime which is designated as θ^o and can be detected at the very beginning of the test. Features in the cycling response can be used to distinguish the FOPDT from SOPDT dynamics. For example, in case of FOPDT process, T_p equals θ^o or θ . The same equality does not apply to the SOPDT case. In a relay feedback test, two measured quantities, A_θ/A and θ/T_p , are used to characterize the effect of the apparent deadtime. These two quantities, as mentioned earlier, are functions of $\bar{\tau}$ and ζ . To explore their functional relations, simulations of relay feedback tests on the standard SOPDT processes covering wide range of $\bar{\tau}$ (in dimensionless form) and ζ are carried out. Results of A_θ/A and θ/T_p for underdamped SOPDT processes are plotted as a graph as shown in Fig. 3(a), using $\bar{\tau}$ and ζ as parameters. Each pair of the two measured quantities corresponds to a point in the graph, where a specific pair of values for $\bar{\tau}$ and ζ can be found. As shown in the figure, it is difficult to read $\bar{\tau}$ and ζ from the figure. In order to make each curve in Fig. 3(a) more readable, the coordinate is rotated through the following transformation.

$$\begin{aligned} X &= \frac{\theta}{T_p} \cos(\pi/3) - \frac{A_\theta}{A} \sin(\pi/3) \\ Y &= \frac{\theta}{T_p} \sin(\pi/3) + \frac{A_\theta}{A} \cos(\pi/3) \end{aligned} \quad (13)$$

The results are plotted in Fig. 3(b). Moreover, for applying these data efficiently, two artificial neural networks (ANN) are constructed. The network architecture is as shown in Fig. 4. These two neural networks are fed with X and Y , and compute $\bar{\tau}$ and ζ , respectively. Each network consists of feedforward net with one input layer, one hidden layer, and one output layer. The sigmoid function f_i is used in an error backpropagation technique to minimize the error between prediction and target values.

With these two networks, estimation of the apparent deadtime can be proceeded. The estimation makes uses of the phase criterion in Eq.(7). Notice that three unknowns are required to satisfy at least four functional relations (i.e. Eqs.(3)-(6) or Eqs.(5)-(8)), and iterative check is thus necessary to find the solution in a least-squares sense. By solving Eqs.(5)-(7), a unique solution for $\bar{\tau}$, ζ and θ can be found. But, the resulting solution may not necessarily satisfy Eq.(8).

The final solution needs further iterative procedures. To satisfy the extra Eq.(8), it is found that manifold in the space of τ and ζ results from the relation of the following:

$$\tan^{-1}\left(\frac{2\omega_u\tau\zeta}{1-\omega_u^2\tau^2}\right)=\pi-\omega_u\theta \quad (14)$$

With ω_u and θ being fixed, there are many pairs of τ and ζ that satisfy Eq.(7), and one of these pairs would make Eq.(8) satisfied.

With the theory presented above, the algorithm for the estimation of apparent deadtime can be made in a simpler way as the following:

1. Starting from a guessed value of θ , which is initially taken as θ^o .
2. The values of X and Y are calculated and fed into two networks. Then, parameters $\bar{\tau}$ and ζ are computed, and check if Eq.(7) holds. The procedure proceeds iteratively by increasing the guess value of θ until θ equals T_p .
3. When, at certain value of guessed θ , Eq.(7) holds true, the resulting guess value θ is taken as the estimated value of apparent deadtime.
4. If, until the guessed value of θ exceeds T_p and no candidate solution is found, the underdamped SOPDT model is not good for describing the dynamics of the process. As a result, model of FOPDT or overdamped SOPDT should be used.

- *Process Classification for modeling*

In general, processes with SOPDT dynamics, which are overdamped or slightly underdamped, are sometimes identified with FOPDT models for controller design without significant difference in performance. It is thus curious to know under what condition can an SOPDT process has controller parameters in terms of an FOPDT parameterization. The FOPDT parameters in terms of ultimate gain and ultimate frequency can be written as:

$$\begin{aligned} \tau &= \frac{\sqrt{K_u^2-1}}{\omega_u} \\ \theta &= \frac{\pi - \tan^{-1}\left(\sqrt{K_u^2-1}\right)}{\omega_u} \end{aligned} \quad (15)$$

where $K_u = k_p k_{cu}$. The result in Eq.(15) indicates that it is necessary with $K_u > 1$. As shown in Fig. 5, K_u of SOPDT processes is plotted against θ/τ using ζ as a parameter. It is found that $K_u > 1$ happens when $\zeta \geq 0.7$ (accurately, $\zeta \geq 1/\sqrt{2}$). Thus, the uses of FOPDT or SOPDT for modeling are discriminated using $\zeta = 1/\sqrt{2}$ as a boundary. As mentioned earlier, from the ATV test, it provides $A/k_p h$ and P_u/θ which are functions of $\bar{\tau}$ and ζ . As shown in Fig. 6, there are two curves that correspond to SOPDT processes with $\zeta = 0.7$ (curve A) and true FOPDT processes (curve B). Curve A and curve B are found to be represented, respectively,

by the following equations:

- Curve A $\Omega = 0.465\Lambda^3 - 2.002\Lambda^2 + 0.958\Lambda - 0.007$ (16)

- Curve B $\Omega = 30.93\Lambda^3 - 56.78\Lambda^2 + 29.03\Lambda - 4.51$ (17)

where $\Omega = \log(A/k_p h)$ and $\Lambda = \log(P_u/\theta)$. These two curves divide the graph of Fig. 6 into

two zones. One is between the curve A and curve B (i.e. Zone I) that represents the feasible region for using parameterization of FOPDT due to $\zeta \geq 0.7$, and the other region above curve A (i.e. Zone II) that represents the feasible region to use parameterization of underdamped SOPDT.

Thus, once k_p and the apparent deadtime θ are obtained, the normalized value of $A/k_p h$ and

P_u/θ can be calculated. Then, compare the resulting value of $\log(A/k_p h)$ with the one calculated from Eq.(16). If the former is smaller, then this process is classified into the group (*Group I*) where Eq.(15) applies compute FOPDT parameters. Otherwise, the process is classified into the other group (*Group II*) where the SOPDT parameters are computed from the ultimate information as the following:

$$\tau = \frac{\sqrt{1 + K_u \cos(\omega_u \theta)}}{\omega_u}$$

$$\zeta = \frac{K_u \sin(\omega_u \theta)}{2\sqrt{1 + K_u \cos(\omega_u \theta)}}$$
(18)

- *Case Study*

In order to illustrate the above identification procedures, a few examples are used for simulation. The results are summarized in Table 1.

Table 1. Results of identification using relay feedback test

No.	Process	A	P_u	k_p	k_{cu}	θ	Classification
1	$\frac{e^{-1.5s}}{(s+1)^5}$	0.72	12.14	1.01	1.81	2.91	FOPDT
2	$\frac{(0.5s+1)e^{-s}}{(s+1)^2(2s+1)}$	0.35	6.56	1.0	3.74	1.32	FOPDT
3	$\frac{e^{-2s}}{(9s^2 + 2.4s + 1)(s+1)}$	1.17	15.90	1.0	1.11	2.72	SOPDT

Conclusions

In this project, for the purpose of performance assessment, a new identification method using the relay feedback test is proposed. The identification considered the effective damping factor for classifying the process into one of two groups, FOPDT and SOPDT. In either case,

besides parameters k_p and θ , the model parameters are given in terms of ultimate gain and ultimate frequency obtained from a constant cycle. These parameters can be estimated within one relay feedback experiment. Two ANNs are constructed to enhance the estimation of apparent deadtime. The identified models can be used not only for performance assessment but also for controller tuning. It becomes an auto-tuning system and can improve control performance effectively. In the next project, the method will be extended to multivariable processes to deal with the performance assessment of multi-loop control systems.

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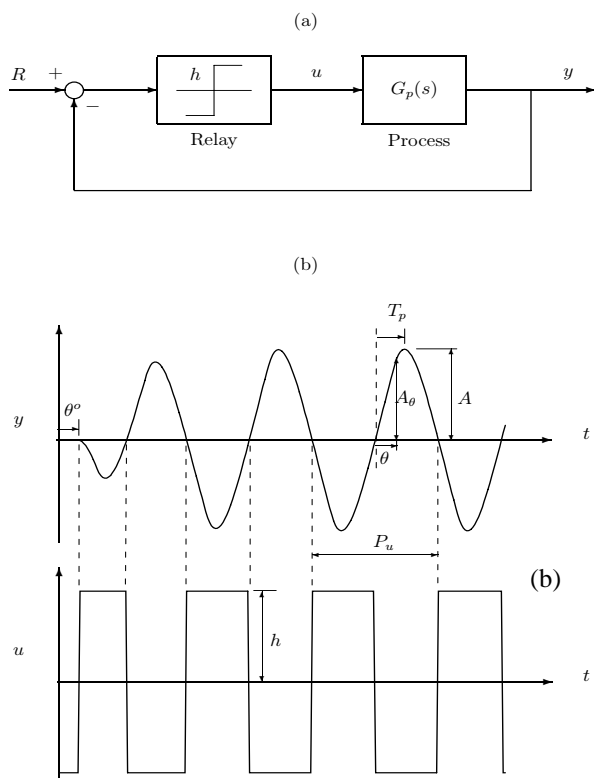


Fig. 1. (a) Block diagram of a relay feedback system (b) Response curves in relay feedback test

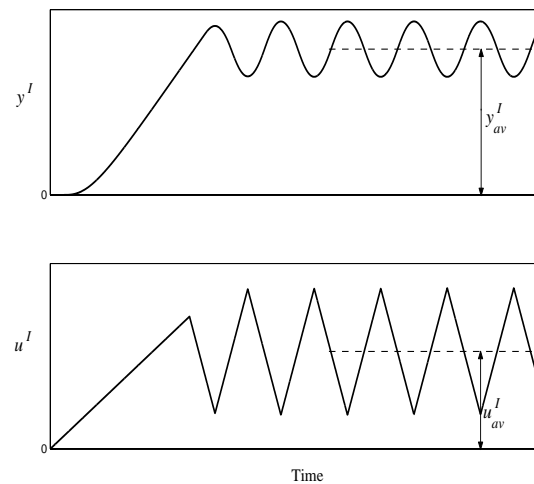


Fig . 2. Typical curves of y^I and u^I in proposed relay feedback test

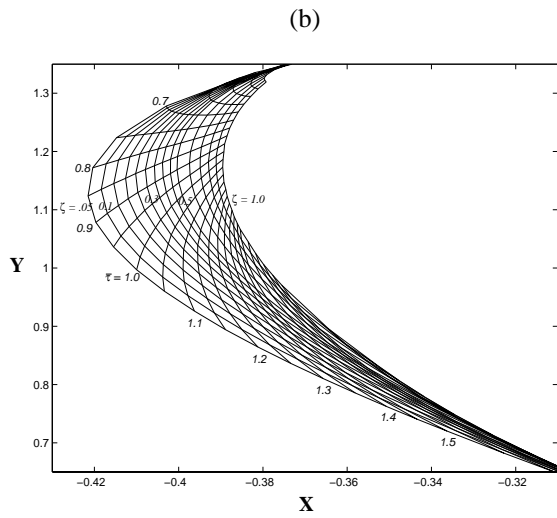
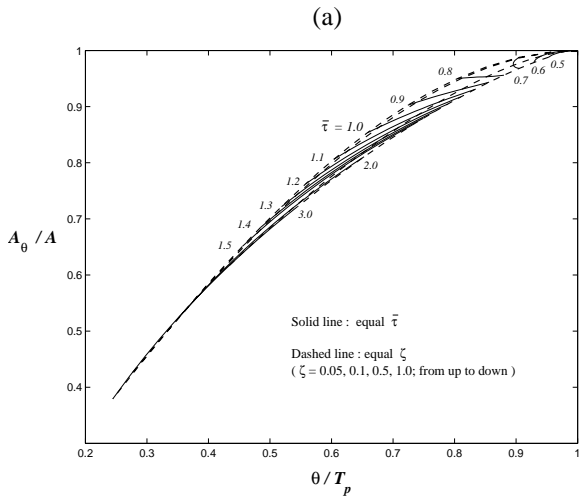


Fig. 3. Results of A_θ/A and θ/T_p in the relay feedback tests for SOPDT processes (a) original (b) transformed

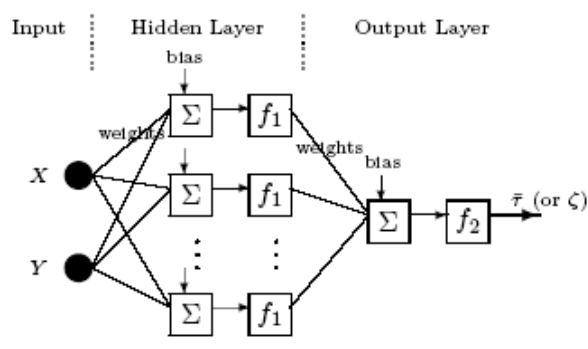


Fig. 4. Neural network architecture

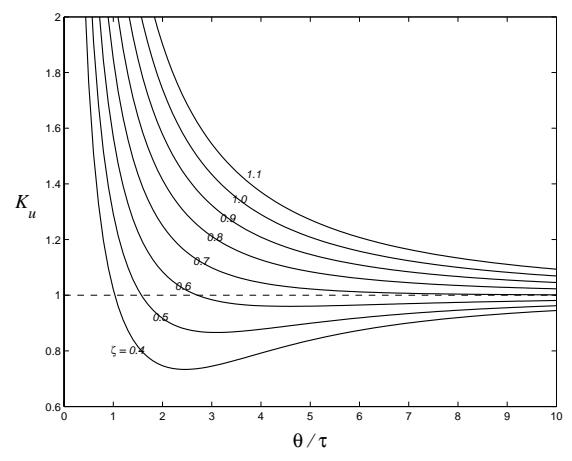


Fig. 5. K_u for different SOPDT processes

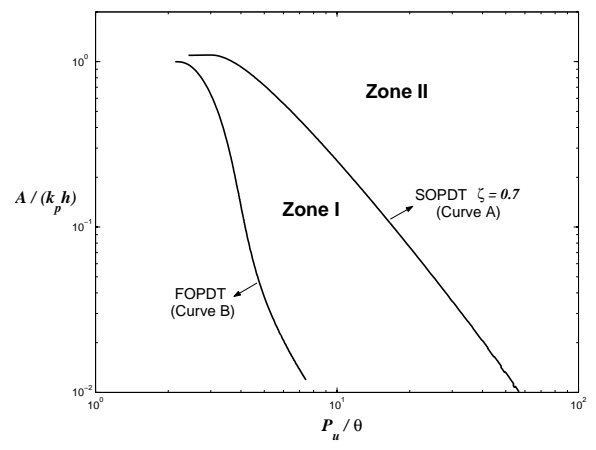


Fig. 6. Curves for process classification